



# AAiT

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**Addis Ababa  
Institute of Technology  
School of Civil and  
Environmental Engineering**

**Water Distribution Modelling  
Lecture By Fiseha Behulu (PhD)**

# Lecture-5: Water Hammer Theory

Prepared By

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2020



# Contents of the Course

1. Components of Water Supply
2. Basic Principles of Pipe Flow (Hydraulics)
3. The Modeling Theory
4. Model Calibration
5. Optimization in WDS
- 6. Water Hammer Theory**
7. Water Supply Project Design (Application of Tools)

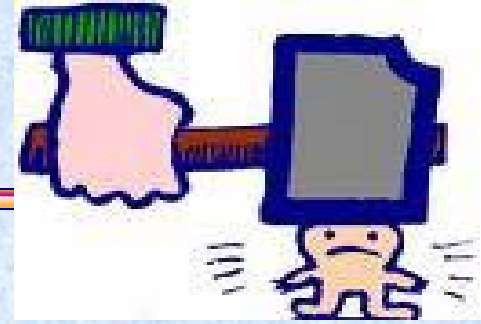
# Water Hammer



- Basic phenomenon
- Modelling
- Mitigating measures



# Water Hammer - problems

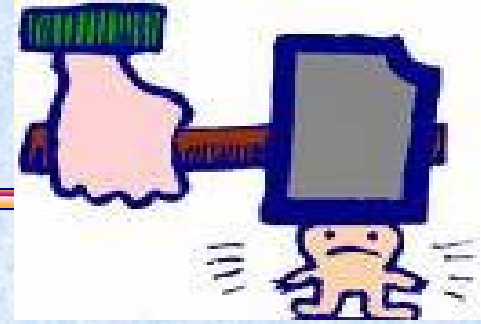


## □ Learning objective

- Understand the transient phenomenon in water distribution system design.
- Identify system which need transient analysis
- Avoid dangerous and costly blunders in designing pipe line system
- Evaluate corrective measures for problems
- Explain the influence of specific hardware on water hammer



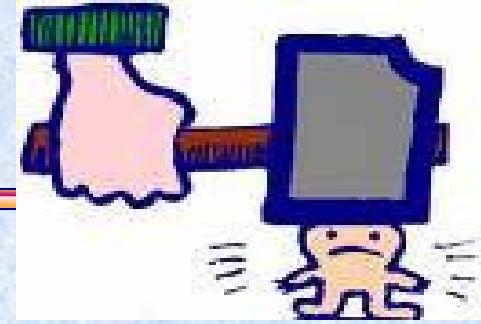
# Water Hammer - problems



**Pipe burst during commissioning**



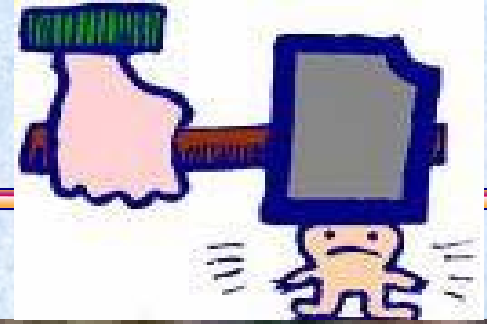
# Water Hammer - problems



**Check valve closure  
forms severe motion  
of pipes**



# Water Hammer - problems

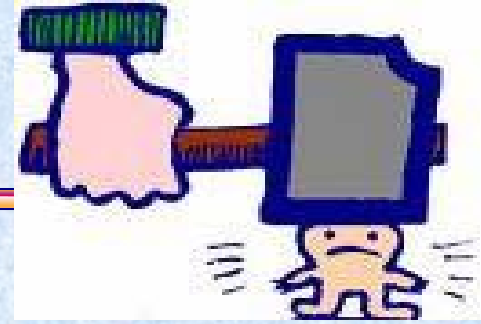


**Collapsing of pipe  
due to negative  
pressure**





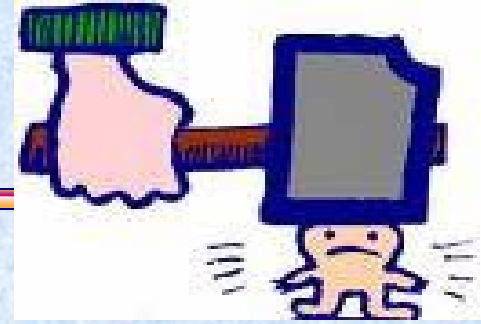
# Water Hammer - problems







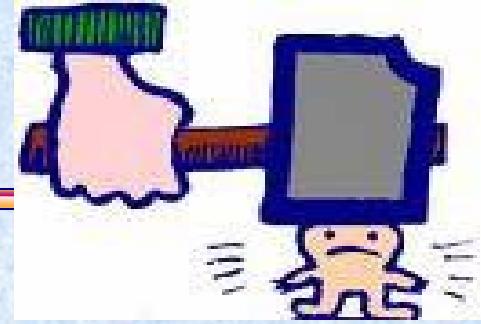
# Water Hammer - Definition



- Momentary increase in pressure , which occurs in a water system when there is a sudden change of direction or velocity of water (Lahlou,2003).



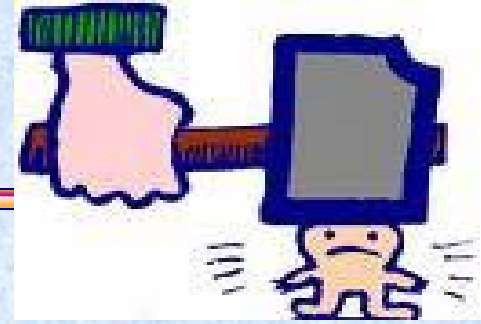
# Water Hammer – the origin



- ❑ Changes in the fundamental flow values at any instant.
  - Pressure
  - Flow
- ❑ Exchange of kinetic and potential energy
  - Velocity changes  $\Leftrightarrow$  pressure changes



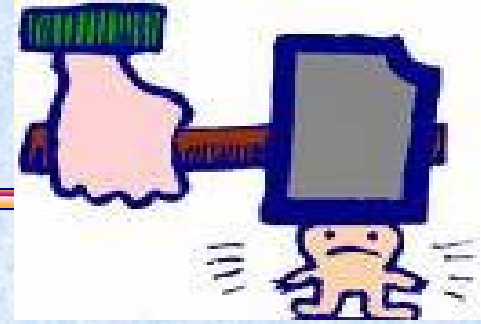
# Water Hammer- concept



- ❑ Changes propagate through the pipe system as high speed waves
  - Water hammer
  - Surges
    - But surge is a lesser form of water hammer. A slow motion of mass oscillation of water caused by internal pressure fluctuation in the system



# Water Hammer- concept



- ❑ Evaluating a hydraulic transient involves determining the values during the time interval  $T_t$  of the functions  $V(x, t)$  and  $p(x, t)$  that result from a flow control operation performed in a time interval  $T_M$ .



# Water Hammer – Physical Principles



**1** Valve closed - water still



**2** Valve open - moving water

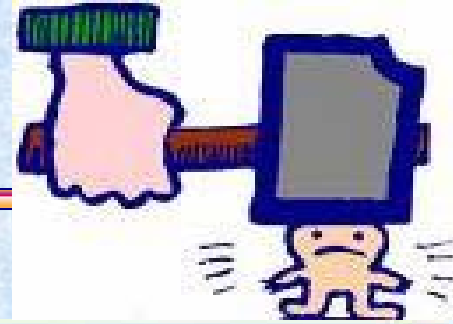


**3** Valve closes - **WATER HAMMER**

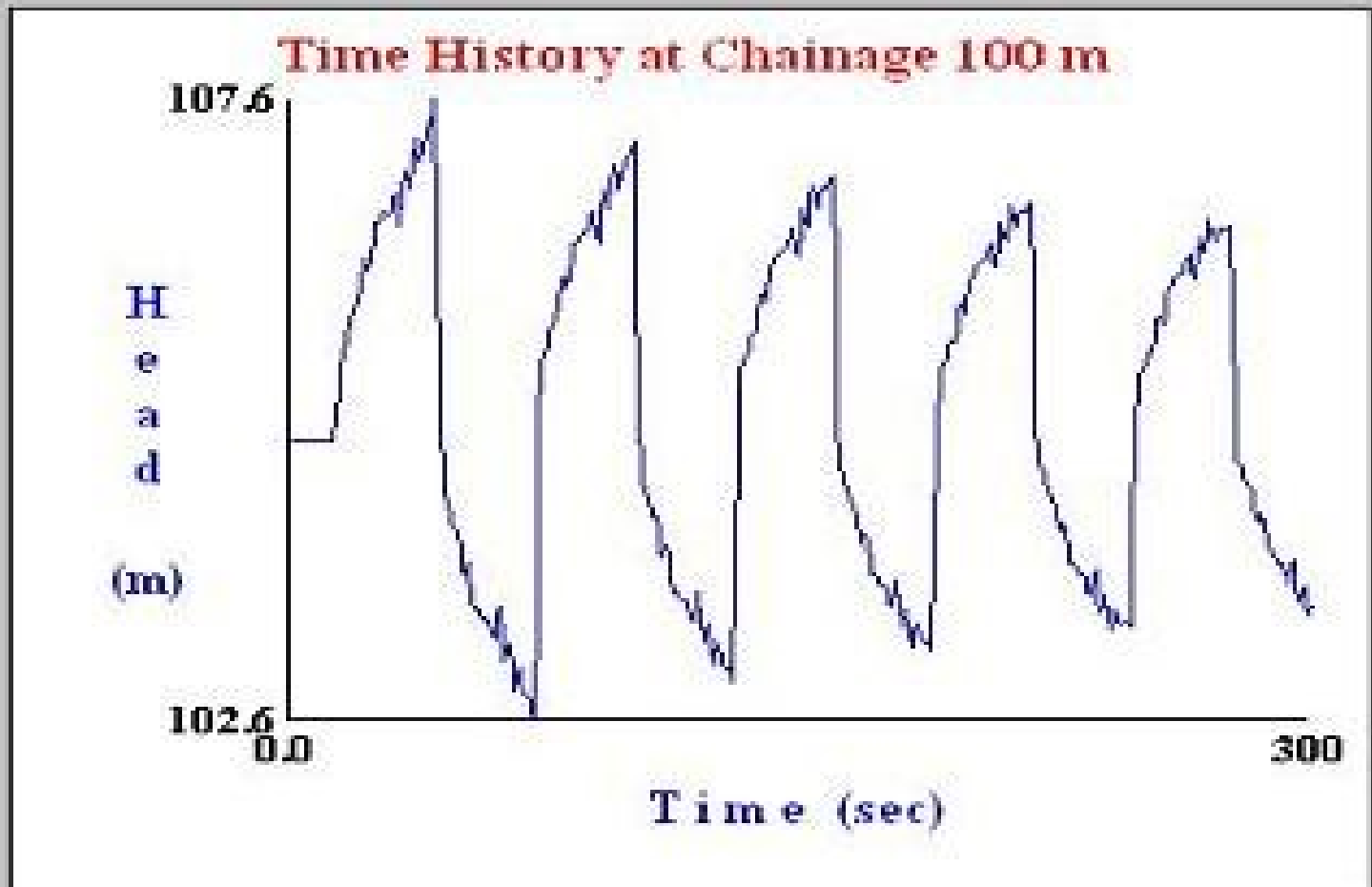




# Water Hammer - Phenomenon

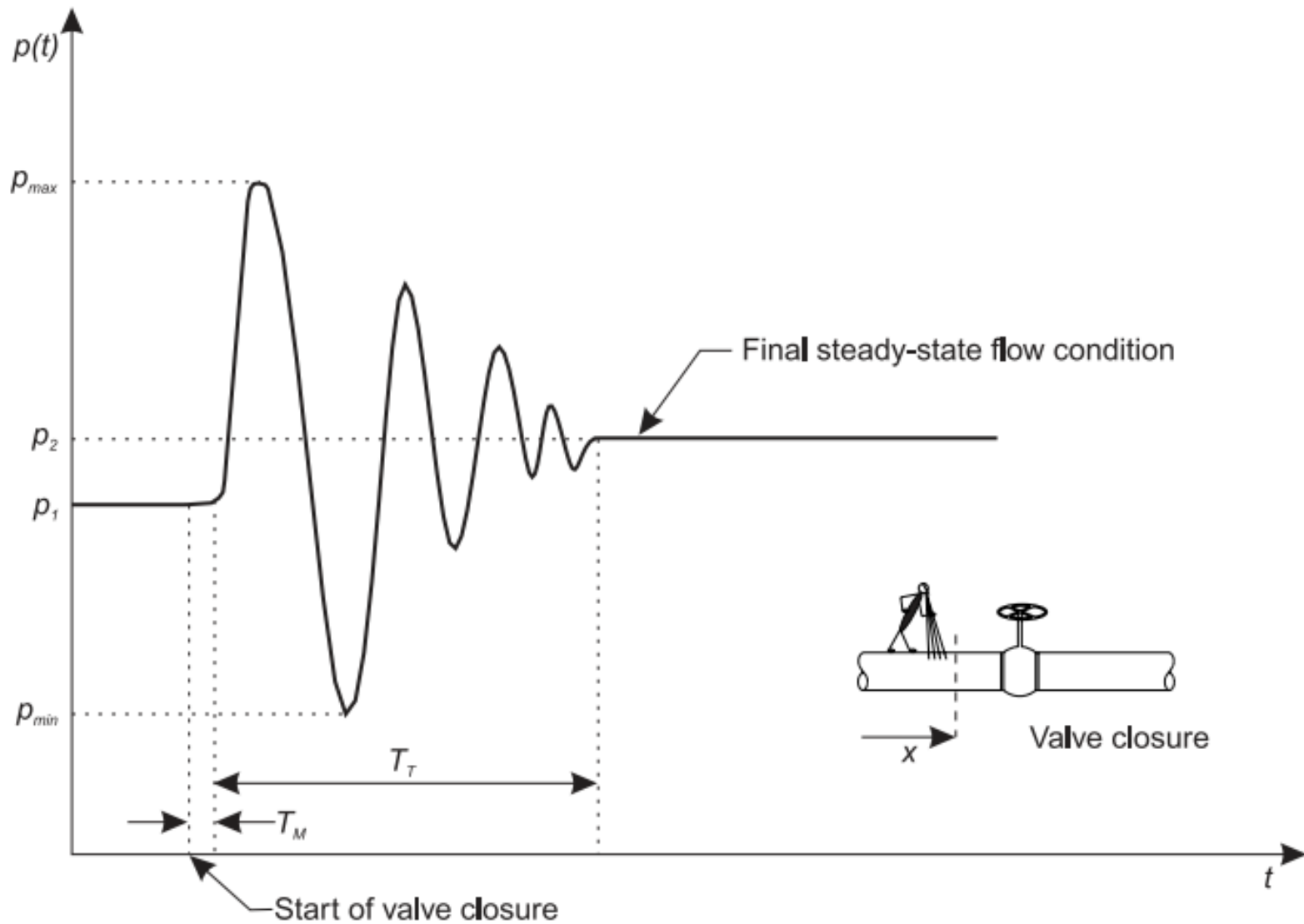


Water Hammer Simulation



Close

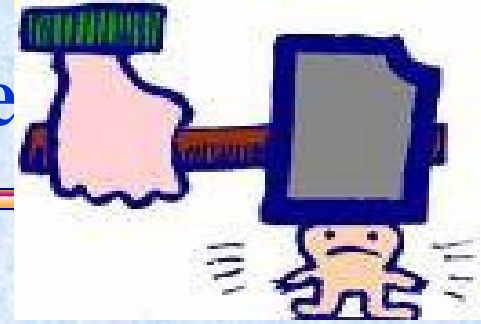




Hydraulic Transient at Position  $x$  in the system (Walski, Page 575)



# Water Hammer- conce



- ❑ Phenomenon reflections
  - High pressure
  - Low pressure (cavitations)



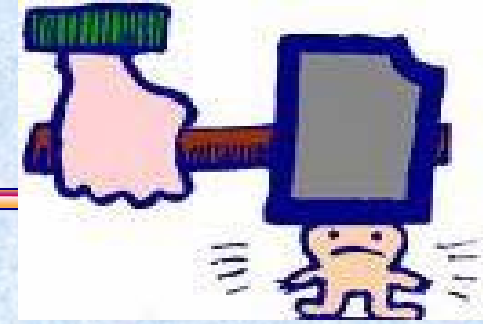
# Water Hammer- Cavitation



- Pressure below a certain level
- Variants
  - Gaseous cavitation
    - Dissolved gases ( oxygen, carbon dioxide)
    - Small gas pocket form in the pipe
  - Vaporous cavitation (column separation)
    - Pressure below the vapor pressure of the liquid



# Water Hammer- Cavitation



- Vaporous cavitation (column separation)
  - Vaporization of the water itself
  - Vapor pocket formation and collapse
  - Result in pipe flexure



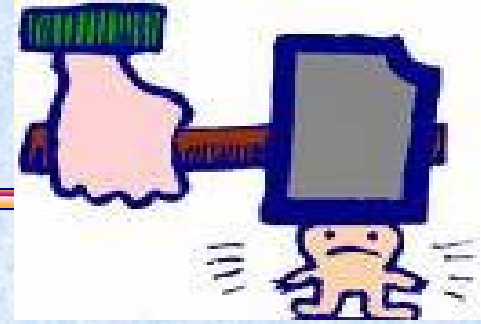
# Significance



If transient pressures are excessively high, the pressure rating of the pipeline may be exceeded, causing failure through pipe or joint rupture, or bend or elbow movement. Excessive negative pressures can cause a pipeline to collapse or groundwater to be

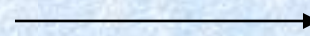


# Water Hammer - problems



- ❑ Damage to

- Pipes
- Fittings and valves



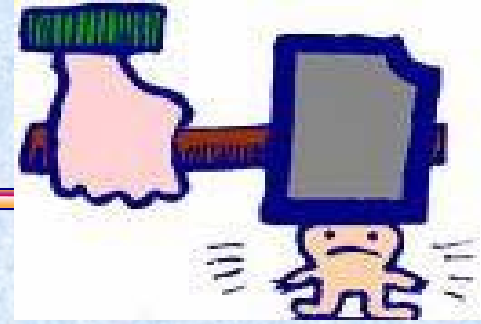
**System failure**

- ❑ Water quality problems





# Water Hammer - causes

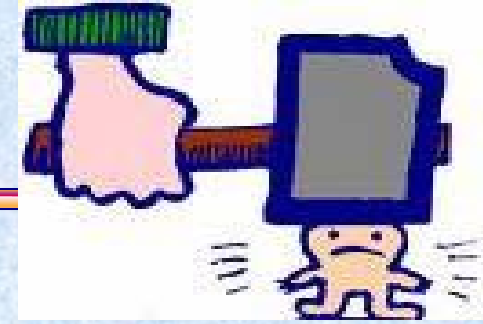


- ❑ System design variable's fluctuation
  - Pressure and flow change
  - Demand fluctuations, and
  - Tank level changes





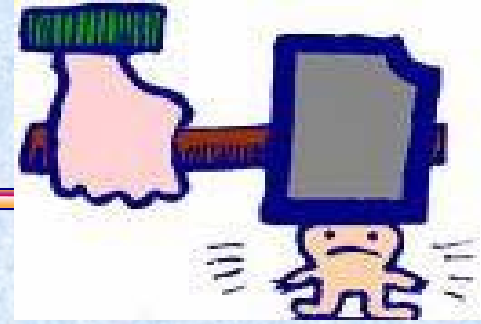
# Water Hammer - causes



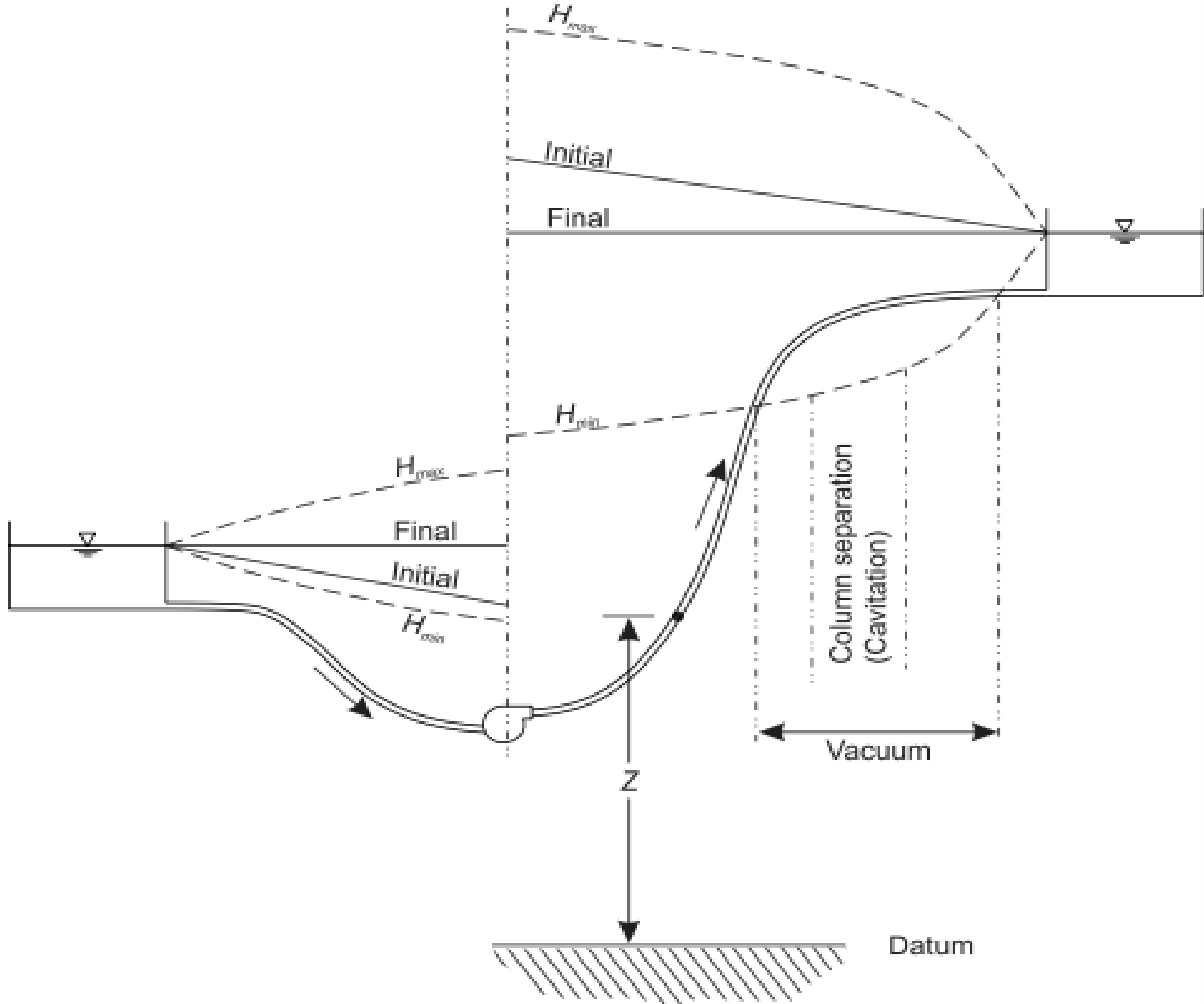
- ❑ Unforeseen events
  - Power outage
  - Equipment malfunction
- ❑ Operational issues
  - Valve closure
- ❑ Entrained air and temperature changes



# Water Hammer Evaluation

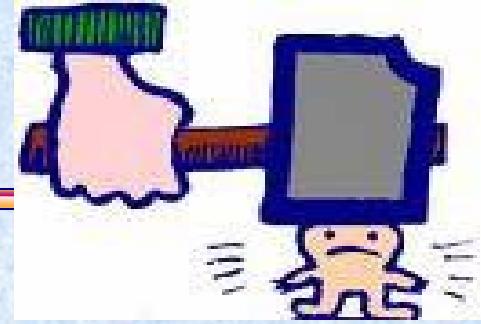


- ❑ Evaluating a system for potential transient impacts involves determining the values of head ( $H_{max}$  and  $H_{min}$ ) at incremental positions in the system. These head values correspond to the minimum and maximum pressures of the transient pressure wave, depicted as  $p_{max}$  and  $p_{min}$





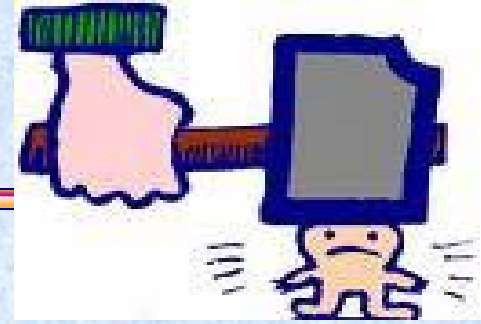
# Water Hammer - physics



- Thrust
  - $V(x,t)$
  - $P(x,t)$
  - Alternatively for  $Q$  and  $H$
- A problem of two unknowns
- Equations
  - Continuity equation
  - Momentum equations



# Water Hammer – physical principles

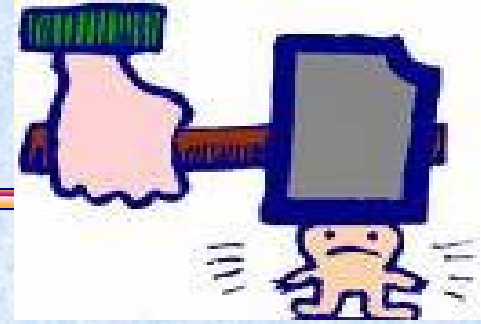


## □ Two modes of analysis

- Rigid model
- Elastic model



# Water Hammer – Rigid Model

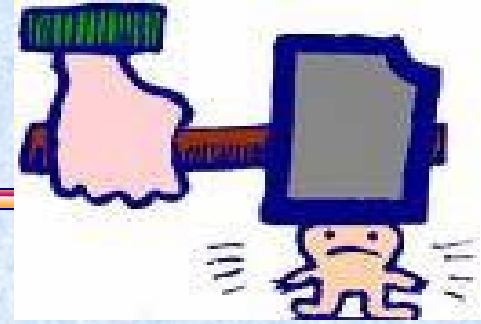


- Rigid models
  - Assumptions
    - pipeline not deformable
    - liquid incompressible
  - Liquid travel mode – mass oscillation

**Flow control operations affect only inertial and frictional aspects**



# Water Hammer – Rigid Model



## □ Basic rigid model

$$H_1 - H_2 = \frac{fL}{2gDA^2} |Q|Q + \frac{L}{gA} \frac{dQ}{dt}$$

where

$H_1$  = total head at position 1 in a pipeline (ft, m)

$H_2$  = total head at position 2 in a pipeline (ft, m)

$f$  = Darcy-Weisbach friction factor

$L$  = length of pipe between positions 1 and 2 (ft, m)

$g$  = gravitational acceleration constant (ft/s<sup>2</sup>, m/s<sup>2</sup>)

$D$  = diameter (ft, m)

$A$  = area (ft<sup>2</sup>, m<sup>2</sup>)

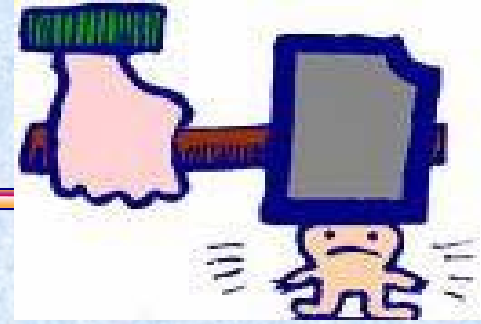
$Q$  = flow (cfs, m<sup>3</sup>/s)

$dQ/dt$  = derivative of  $Q$  with respect to time

**Steady  
state  
-Darcy  
Weisbach  
Otherwise  
Three  
unknowns**



# Water Hammer – physical principles

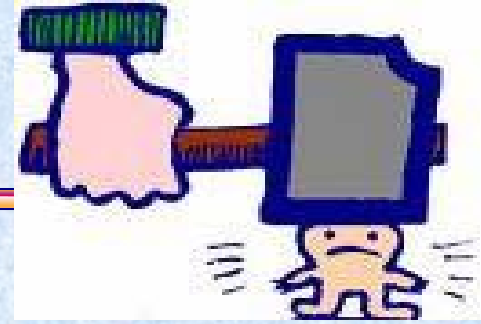


- Then three unknowns need to be determined:
  - $H1(t)$  (the upstream head),
  - $H2(t)$  (the downstream head), and
  - $Q(t)$  (the instantaneous flow in the conduit).
  
- To determine these unknowns, the engineer must know the boundary conditions at both ends of the pipeline.





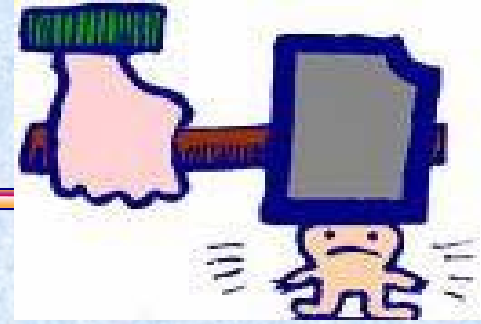
# Water Hammer – Rigid Model



- Limitations
  - Limited in its interpretations of wave propagation caused by flow control operations.
  - Not applicable to rapid changes in flow
- Surge analysis
  - Head changes occur slowly
  - Are minor



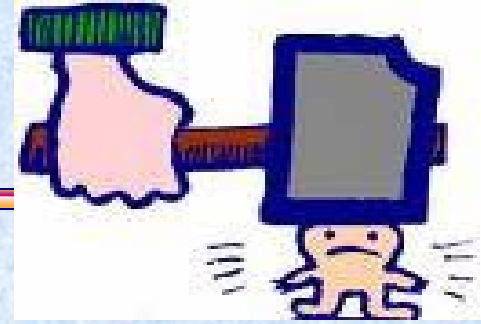
# Elastic Model -



- For short closing interval – Elastic Model
  - Assumptions
    - Liquid compressible
    - Material elasticity
  - Wave propagation phenomenon
  - Wave speed
    - Elasticity of pipeline and fluid



# Elastic Model -

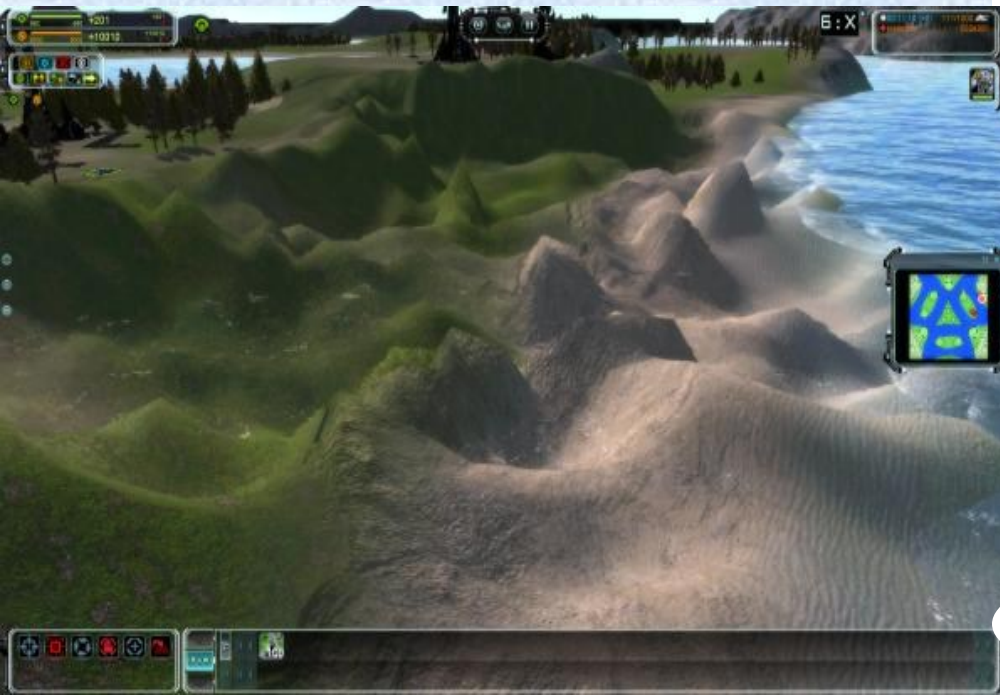


- Elasticity of medium ( liquid)
  - Elasticity coefficient



# Elastic Model -

Force



Deformation



# Elastic Model –



$$E_v = -\frac{dp}{dV/N} = \frac{dp}{(d\rho)/\rho} \quad (13.2)$$

where  $E_v$  = volumetric modulus of elasticity (M/LT<sup>2</sup>)

$dp$  = static pressure rise (M/LT<sup>2</sup>)

$dV/N$  = incremental change in liquid volume with respect to initial volume

$d\rho/\rho$  = incremental change in liquid density with respect to initial density



# Elastic Model



■ **Example – Computing Modulus of Elasticity for a Fluid.** Assume that a 0.26-gal (1-liter) volume of water at ambient temperature with a density of 1.94 slugs/ft<sup>3</sup> (1,000 kg/m<sup>3</sup>) is subjected to a pressure of approximately 290 psi (20 bar). In this case, the volume would decrease by approximately 0.055 in<sup>3</sup> (0.9 cm<sup>3</sup>), or by 0.09%. Compute the modulus of elasticity for water.

Using Equation 13.2, the modulus of elasticity can be computed as

$$E_v = -290 \text{ psi} / -0.0009 = 3.2 \times 10^5 \text{ psi}$$

or

$$E_v = -20 \text{ bars} / -0.0009 = 2.2 \times 10^4 \text{ bars} = 2.2 \times 10^9 \text{ Pa} = 2.2 \text{ GPa}$$



# Elastic Model



A relationship between a liquid's modulus of elasticity and density yields its characteristic wave celerity, as shown in Equation 13.3.

$$a = \sqrt{\frac{E_v}{\rho}} = \sqrt{\frac{dp}{d\rho}}$$

where  $a$  = characteristic wave celerity of the liquid (L/T)

**Case - Rigid pipe system**



# Elastic Model -

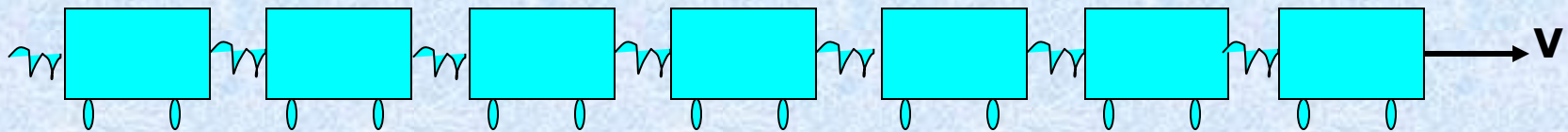
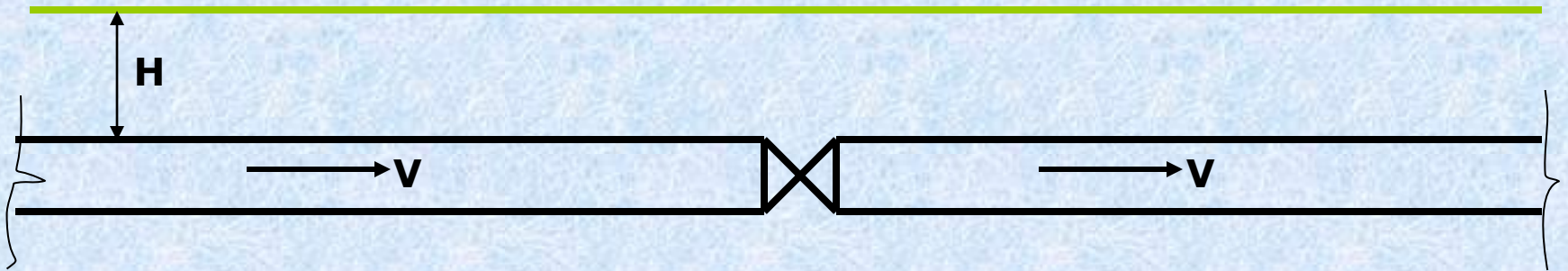
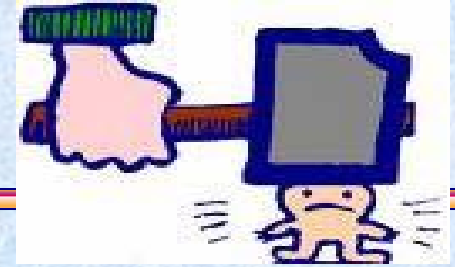


| Medium              | Wave Speed (a) – m/s |
|---------------------|----------------------|
| Water               | 1438                 |
| Air                 | 340                  |
| Water (1% free air) | 125                  |



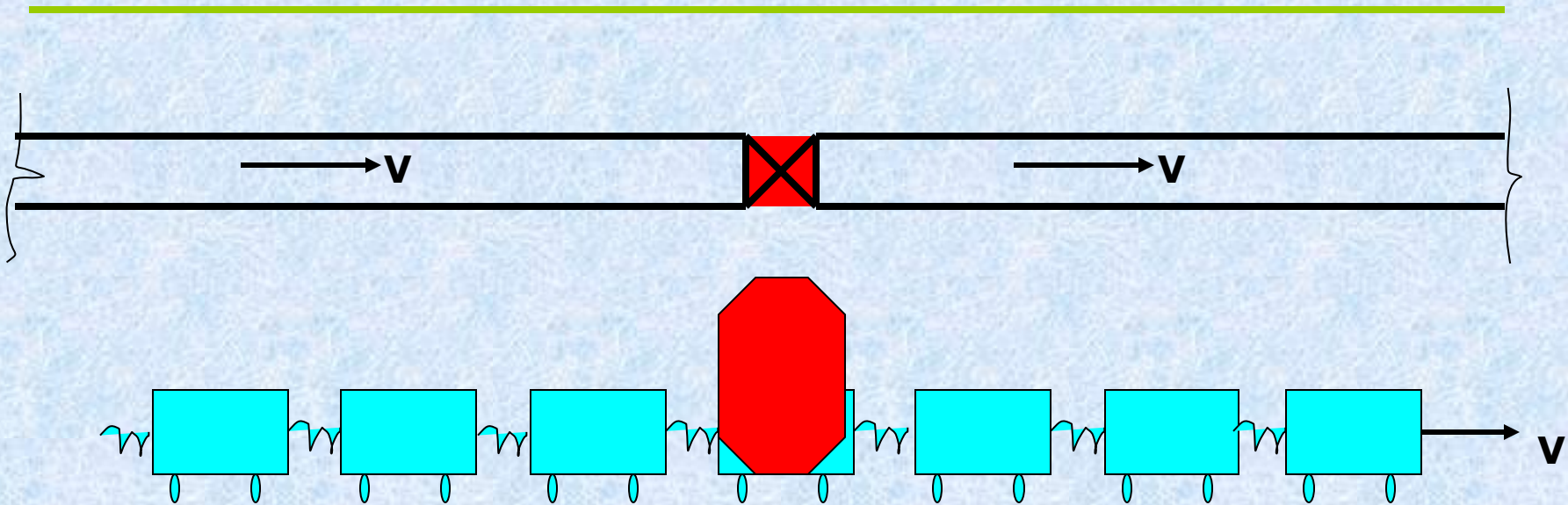
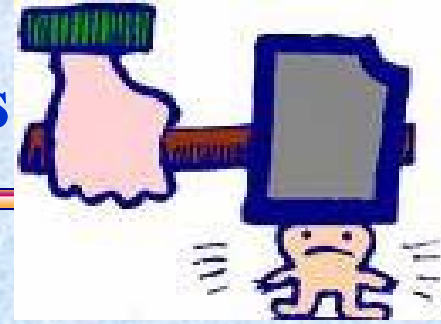


# Water Hammer - physical principles



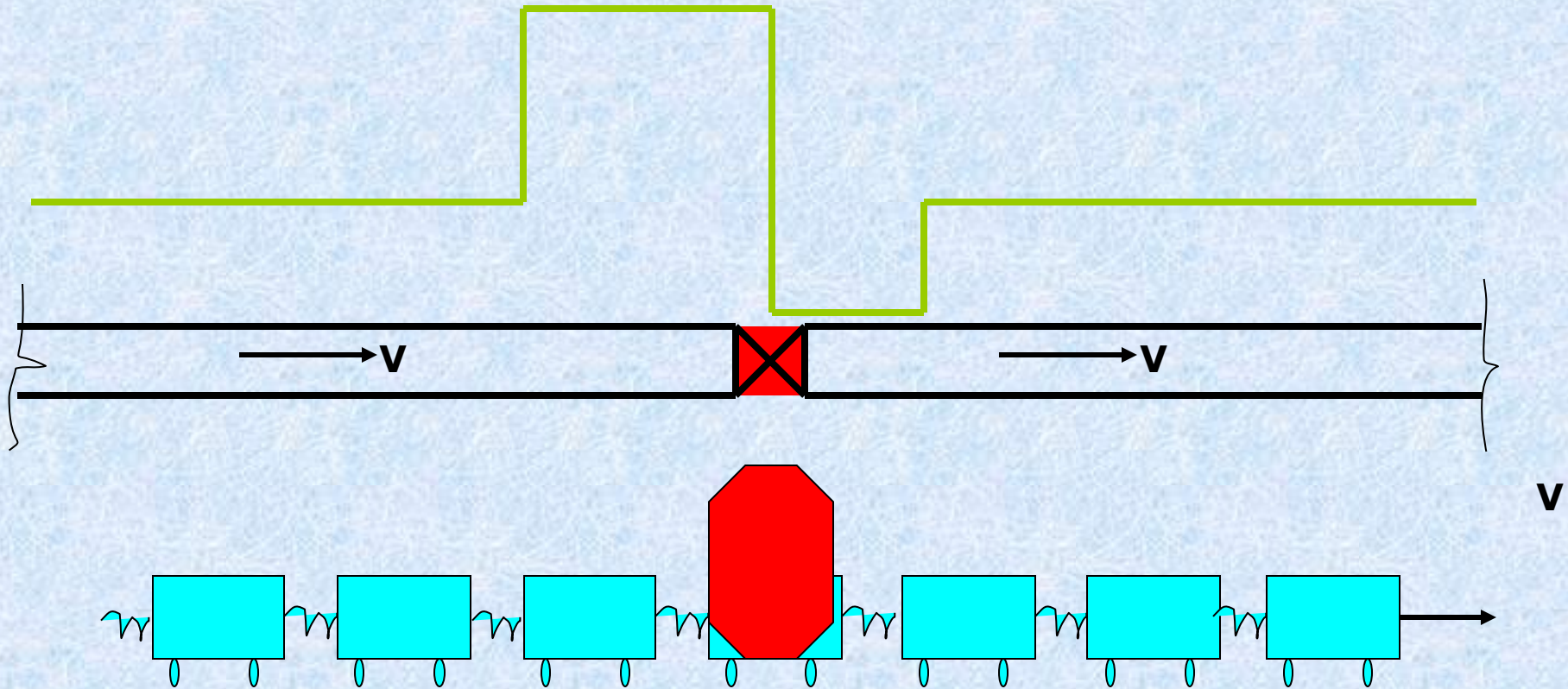


# Water Hammer - physical principles





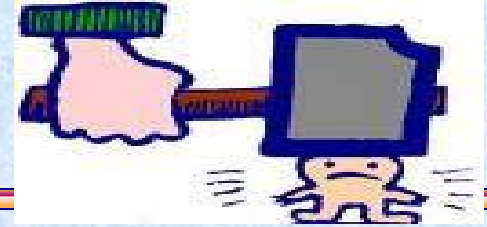
# Water Hammer - physical principles





# Water Hammer

## - physical principles



- Closure - abrupt pressure change

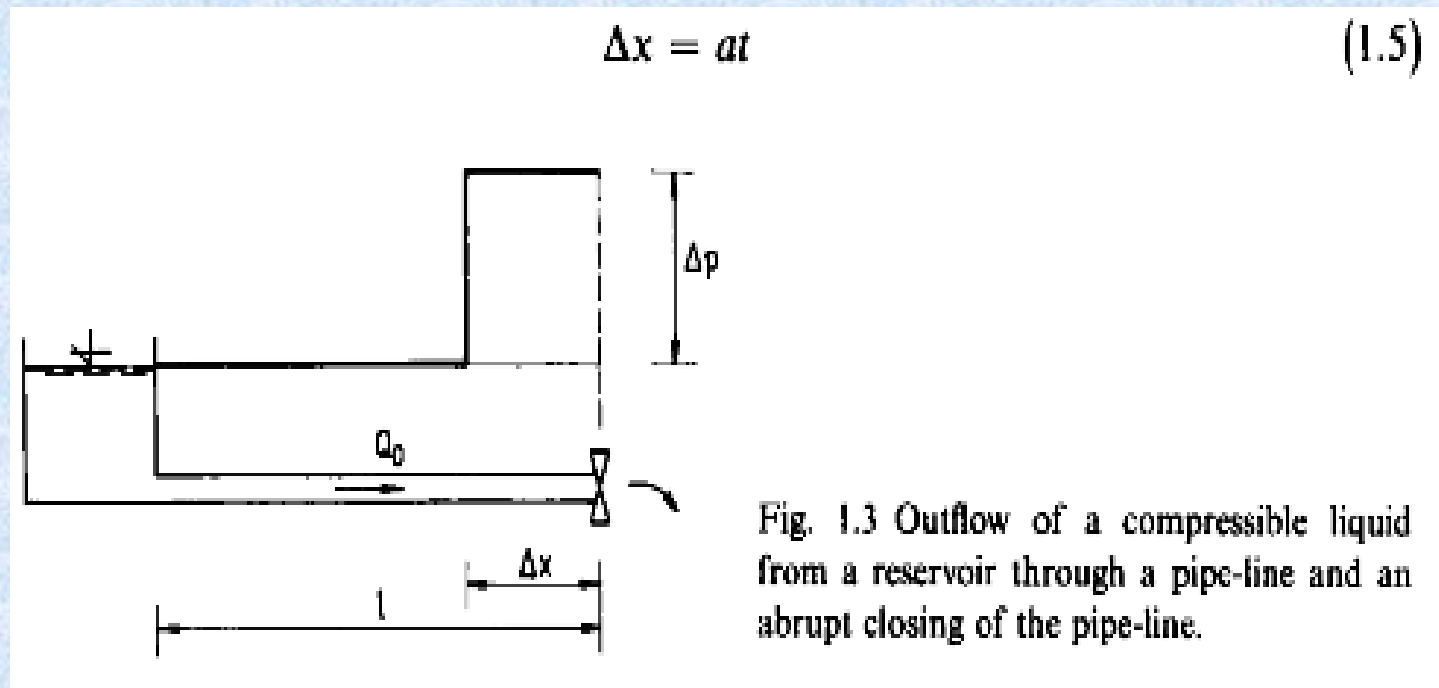
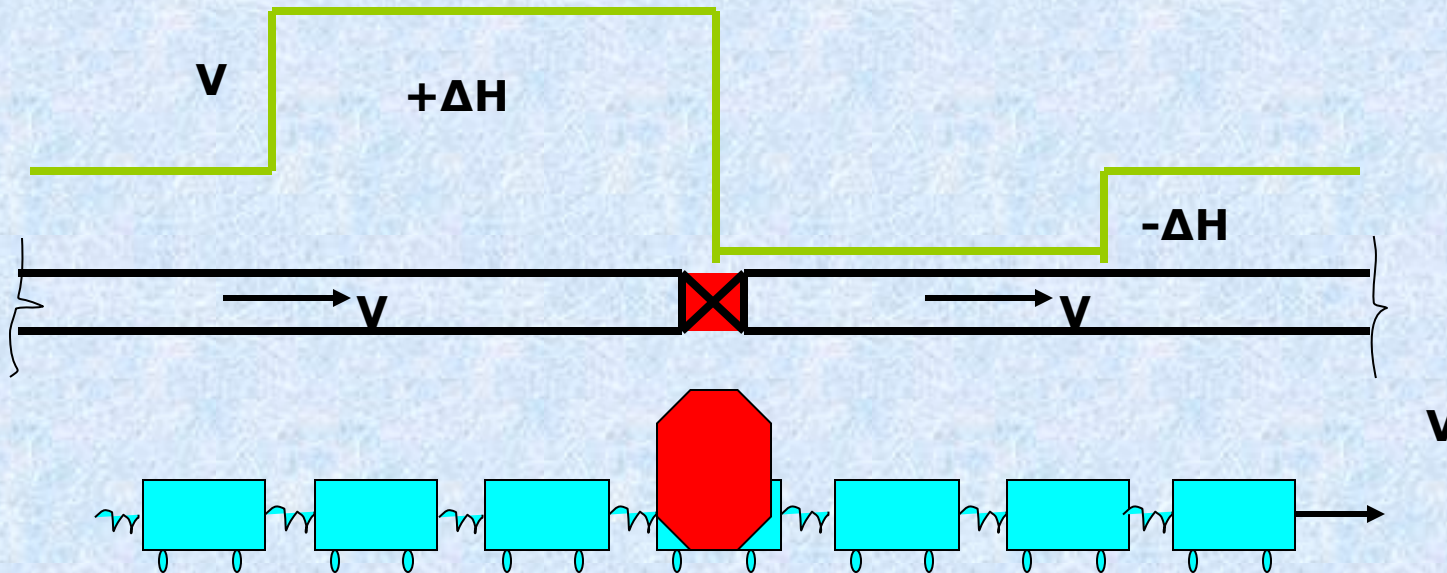


Fig. 1.3 Outflow of a compressible liquid from a reservoir through a pipe-line and an abrupt closing of the pipe-line.



# Water Hammer

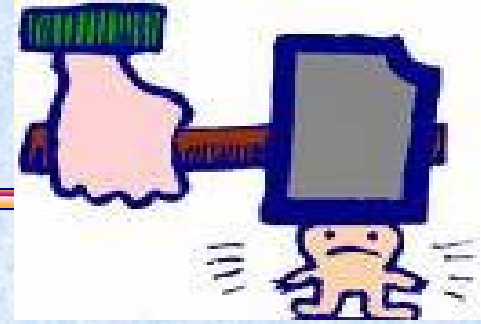
## - physical principles



- Over pressure and negative pressure waves
- Head and velocity related
- pressure waves travel through system



# Equations

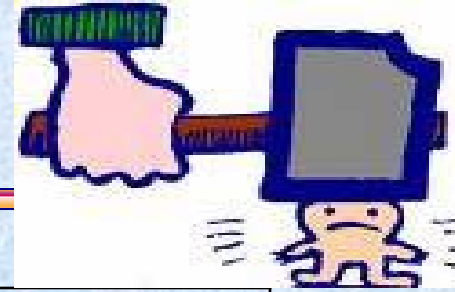


$$\Delta p = -\rho a \Delta V \text{ or } \Delta H = -\frac{a}{g} \Delta V$$

- where
- $\Delta p$  - change in pressure (psi, Pa)
  - $\rho$  - fluid density (slugs/ft<sup>3</sup>, kg/m<sup>3</sup>)
  - $a$  - characteristic wave celerity of the fluid (ft/s, m/s)
  - $\Delta V$  - change in fluid velocity (ft/s, m/s)
  - $\Delta H$  - change in head (ft, m)



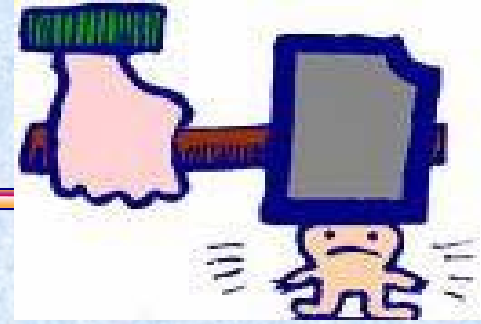
# Water Hammer- physical principles



| a   | $\rho$ | $\Delta V$ | $\Delta P$ |
|-----|--------|------------|------------|
| 980 | 1000   | 0.1        | 98000      |
| 980 | 1000   | 0.2        | 196000     |
| 980 | 1000   | 0.3        | 294000     |
| 980 | 1000   | 0.4        | 392000     |
| 980 | 1000   | 0.5        | 490000     |
| 980 | 1000   | 0.6        | 588000     |
| 980 | 1000   | 0.7        | 686000     |
| 980 | 1000   | 0.8        | 784000     |
| 980 | 1000   | 0.9        | 882000     |
| 980 | 1000   | 1          | 980000     |



# Water Hammer- physical principles







# Water Hammer- physical principles



**Approximate Conversions Between common Pressure Units**

| Pressure Class   | PN | Bar | Meters head | MPa | kPa  | Psi |
|------------------|----|-----|-------------|-----|------|-----|
| A                | 3  | 3   | 30          | 0.3 | 300  | 45  |
| B                | 6  | 6   | 60          | 0.6 | 600  | 90  |
| C                | 9  | 9   | 90          | 0.9 | 900  | 135 |
| D                | 12 | 12  | 120         | 1.2 | 1200 | 180 |
| E                | 15 | 15  | 150         | 1.5 | 1500 | 225 |
| F                | 18 | 18  | 180         | 1.8 | 1800 | 270 |
| No class Defined | 10 | 10  | 100         | 1   | 1000 | 150 |
| No class Defined | 16 | 16  | 160         | 1.6 | 1600 | 240 |
| No class Defined | 20 | 20  | 200         | 2   | 2000 | 300 |
| No class Defined | 25 | 25  | 250         | 2.5 | 2500 | 375 |



# Water Hammer- Demarcation



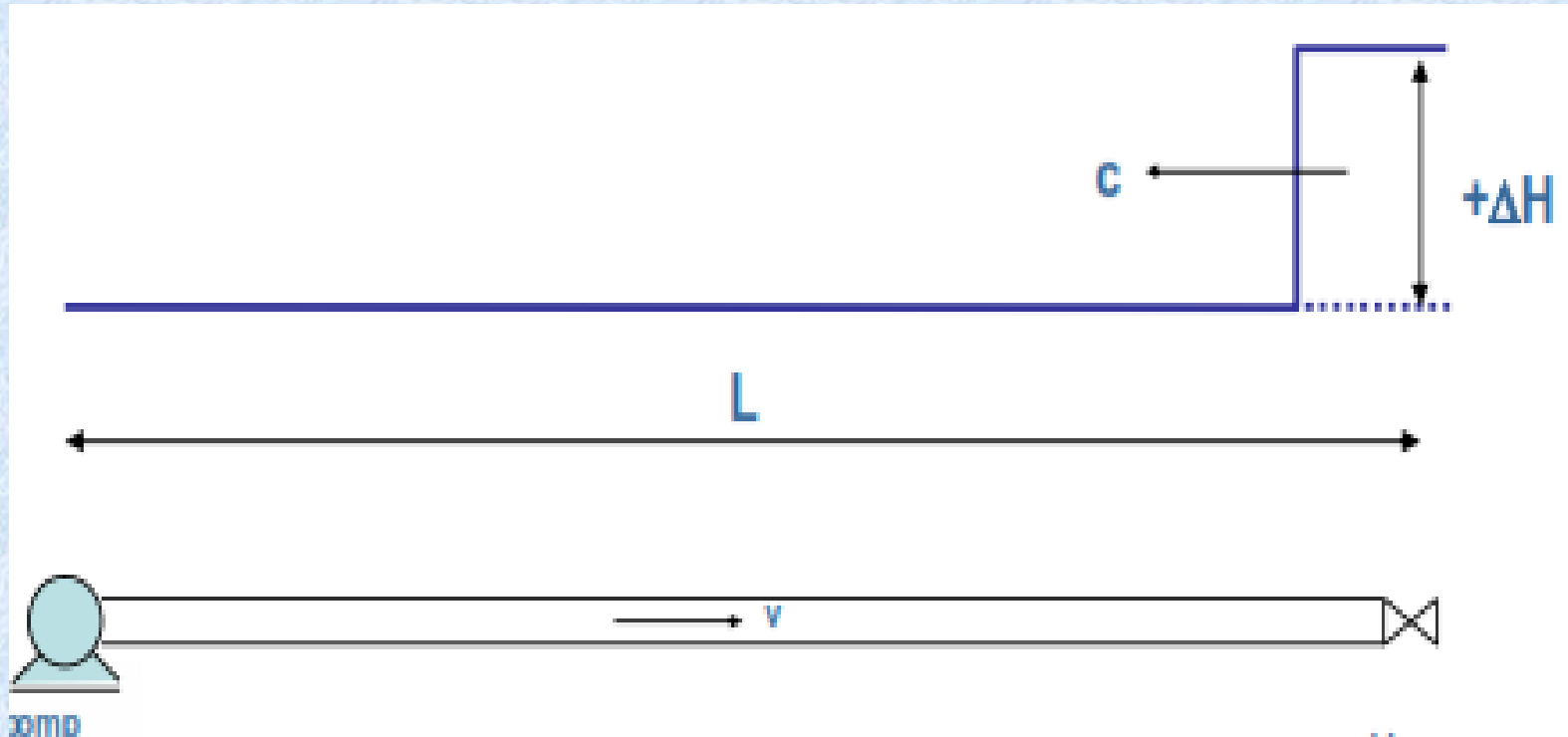
## □ Characteristics Time

<http://www.acs.psu.edu/drussell/Demos/reflect/reflect.html>

- Time for a complete cycle of wave
- Defines the water hammer phenomenon definition

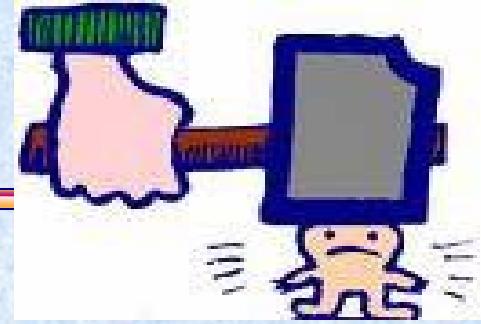


# Water Hammer- Demarcation





# Water Hammer- Demarcation



Classification of flow control operations based on system characteristic time

| Operation Time  | Operation Classification |
|-----------------|--------------------------|
| $T_M = 0$       | Instantaneous            |
| $T_M \leq 2L/a$ | Rapid                    |
| $T_M > 2L/a$    | Gradual                  |
| $T_M \gg 2L/a$  | Slow                     |



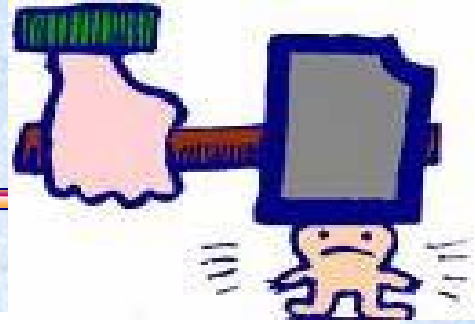
# Water Hammer- phenomenon



- At time  $0 < t < L/a$ , the wave front is moving toward the reservoir. To the right of the front, the water has stopped and the pressure has increased. To the left of the front, the water does not yet “know” that the valve was shut, so it continues to move to the right at the initial head.
- At time  $t = L/a$ , the wave front has reached the reservoir and all the water in the pipe has stopped and is compressed. However, the head in the pipe is above the water level in the reservoir. This difference in head must be relieved, so the water begins to move to the reservoir.
- At time  $L/a < t < 2L/a$ , the wave front moves toward the valve, and water to the left of the front moves toward the reservoir. Water to the right of the front is motionless and is compressed.
- At time  $t = 2L/a$ , the wave front has reached the valve and water is moving away from the valve toward the reservoir. Of course, the water cannot continue to move away from a dead end, so another wave cycle begins.



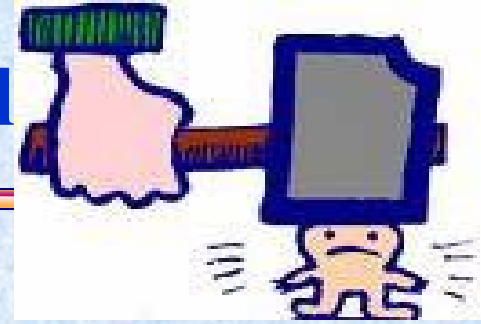
# Water Hammer- phenomenon



- e) At time  $2L/a < t < 3L/a$ , the wave front is moving away from the valve. To the right of the front, pressures are below static pressure and velocity is zero. To the left, velocity continues in the direction of the reservoir, but the pressure is static.
- f) At time  $t = 3L/a$ , the wave has again reached the reservoir. However, the head in the pipe is below the water level in the reservoir and the water is at a low density. Another wave cycle must start.
- g) At time  $3L/a < t < 4L/a$ , the wave is once again moving back toward the valve. This time, the pressure to the left is at the static value and water is moving into the pipe. To the right, velocity is zero and the pressure is below static.
- h) At time  $t = 4L/a$ , the wave has reached the closed valve again and conditions are the same as they were at  $t = 0$ . The wave will start again and would continue indefinitely if not for friction and other energy dissipation mechanisms that will eventually dampen the wave



# Water Hammer – Elastic Model

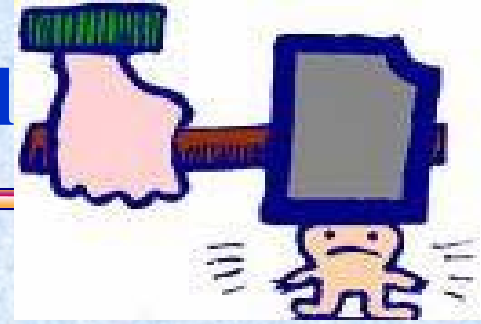


## □ Boundary conditions

- Changes in valve settings, accidental or planned
- Starting or stopping of pumps
- Changes in power demand in turbines
- Action of reciprocating pumps
- Changing elevation of the reservoir
- Vibration of deformable appurtenances such as valves
- Unstable pump or fan characteristics



# Water Hammer – Elastic Model



## □ Joukowski Equation

$$dH = \pm \frac{a}{g} dV = \pm \frac{a}{gA} dQ = \pm B dQ$$

where

$H$  = head (ft, m)

$a$  = characteristic wave speed of the liquid (ft/s, m/s)

$g$  = gravitational acceleration constant (ft/s<sup>2</sup>, m/s<sup>2</sup>)

$V$  = fluid velocity (ft/s, m/s)

$A$  = area (ft<sup>2</sup>, m<sup>2</sup>)

$Q$  = flow (cfs, m<sup>3</sup>/s)

$B$  = characteristic impedance,  $a/gA$  (s/ft<sup>2</sup>, s/m<sup>2</sup>)

**Joukowski:**  $\Delta H = \frac{c}{g} \Delta v$  **or:**  $\Delta p = \rho c \Delta v$





# Water Hammer – Elastic Model



$$a = \sqrt{\frac{\frac{E_v}{\rho}}{1 + \frac{E_v \Delta A}{A \Delta p}}} \quad (13.6)$$

where  $E_v$  = volumetric modulus of elasticity of the fluid (lbf/ft<sup>2</sup>, Pa)

$\Delta A$  = change in cross-sectional area of pipe (ft<sup>2</sup>, m<sup>2</sup>)



# Elastic Model



**Table 13.3** Physical properties of some common liquids

| Liquid       | Temperature<br>(°C) | Bulk Modulus of Elasticity    |            | Density                  |                      |
|--------------|---------------------|-------------------------------|------------|--------------------------|----------------------|
|              |                     | ( $10^6$ lb/ft <sup>2</sup> ) | (GPa)      | (slugs/ft <sup>3</sup> ) | (kg/m <sup>3</sup> ) |
| Fresh Water  | 20                  | 45.7                          | 2.19       | 1.94                     | 998                  |
| Salt Water   | 15                  | 47.4                          | 2.27       | 1.99                     | 1,025                |
| Mineral Oils | 25                  | 31.0 to 40.0                  | 1.5 to 1.9 | 1.67 to 1.73             | 860 to 890           |
| Kerosene     | 20                  | 27.0                          | 1.3        | 1.55                     | 800                  |
| Methanol     | 20                  | 21.0                          | 1.0        | 1.53                     | 790                  |



# Elastic Model

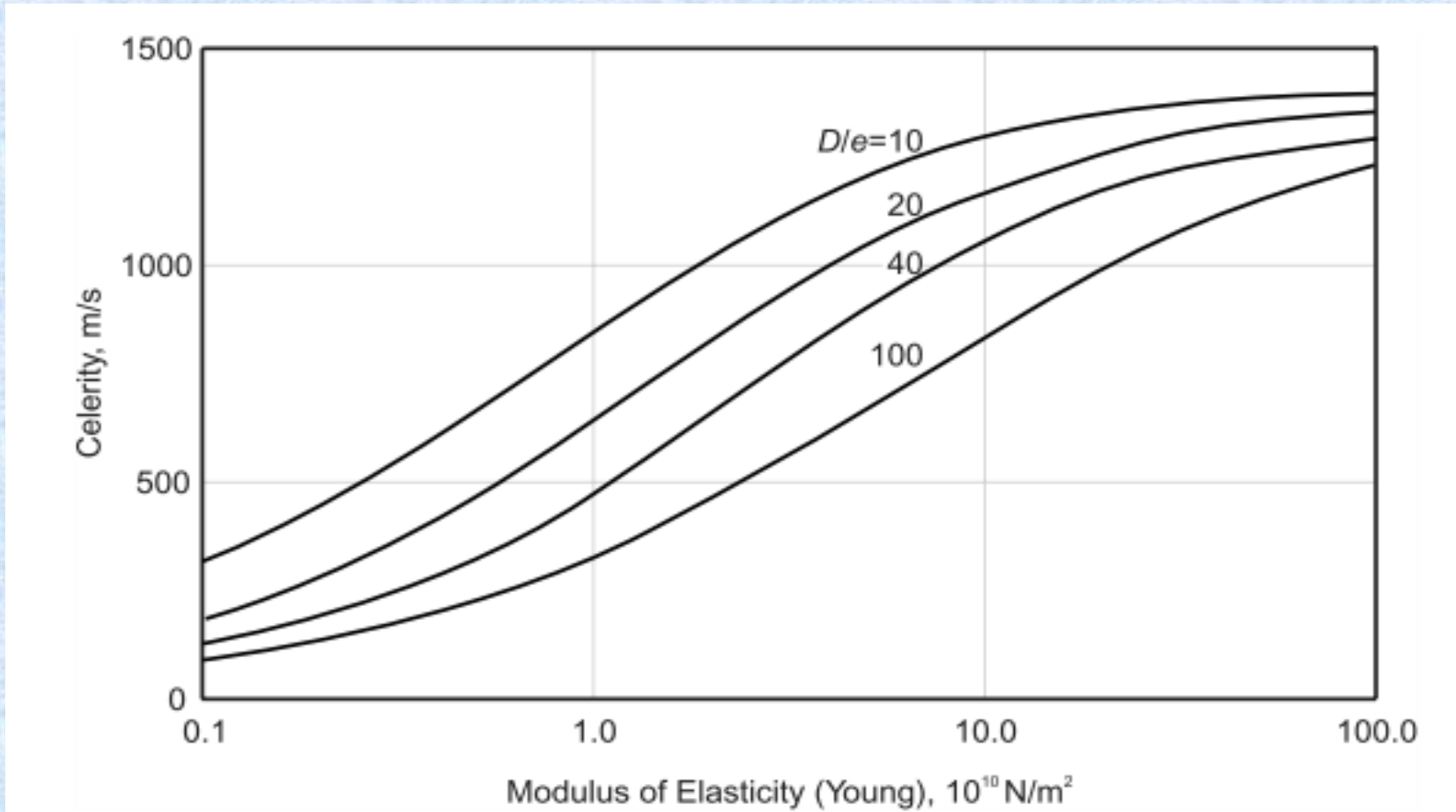


**Table 13.2** Physical properties of some common pipe materials

| Material            | Young's Modulus                |          | Poisson's Ratio, $\mu$ |
|---------------------|--------------------------------|----------|------------------------|
|                     | ( $10^9$ lbf/ft <sup>2</sup> ) | (GPa)    |                        |
| Steel               | 4.32                           | 207      | 0.30                   |
| Cast Iron           | 1.88                           | 90       | 0.25                   |
| Ductile Iron        | 3.59                           | 172      | 0.28                   |
| Concrete            | 0.42 to 0.63                   | 20 to 30 | 0.15                   |
| Reinforced Concrete | 0.63 to 1.25                   | 30 to 60 | 0.25                   |
| Asbestos Cement     | 0.50                           | 24       | 0.30                   |
| PVC (20°)           | 0.069                          | 3.3      | 0.45                   |
| Polyethylene        | 0.017                          | 0.8      | 0.46                   |
| Polystyrene         | 0.10                           | 5.0      | 0.40                   |
| Fiberglass          | 1.04                           | 50.0     | 0.35                   |
| Granite (rock)      | 1.0                            | 50       | 0.28                   |

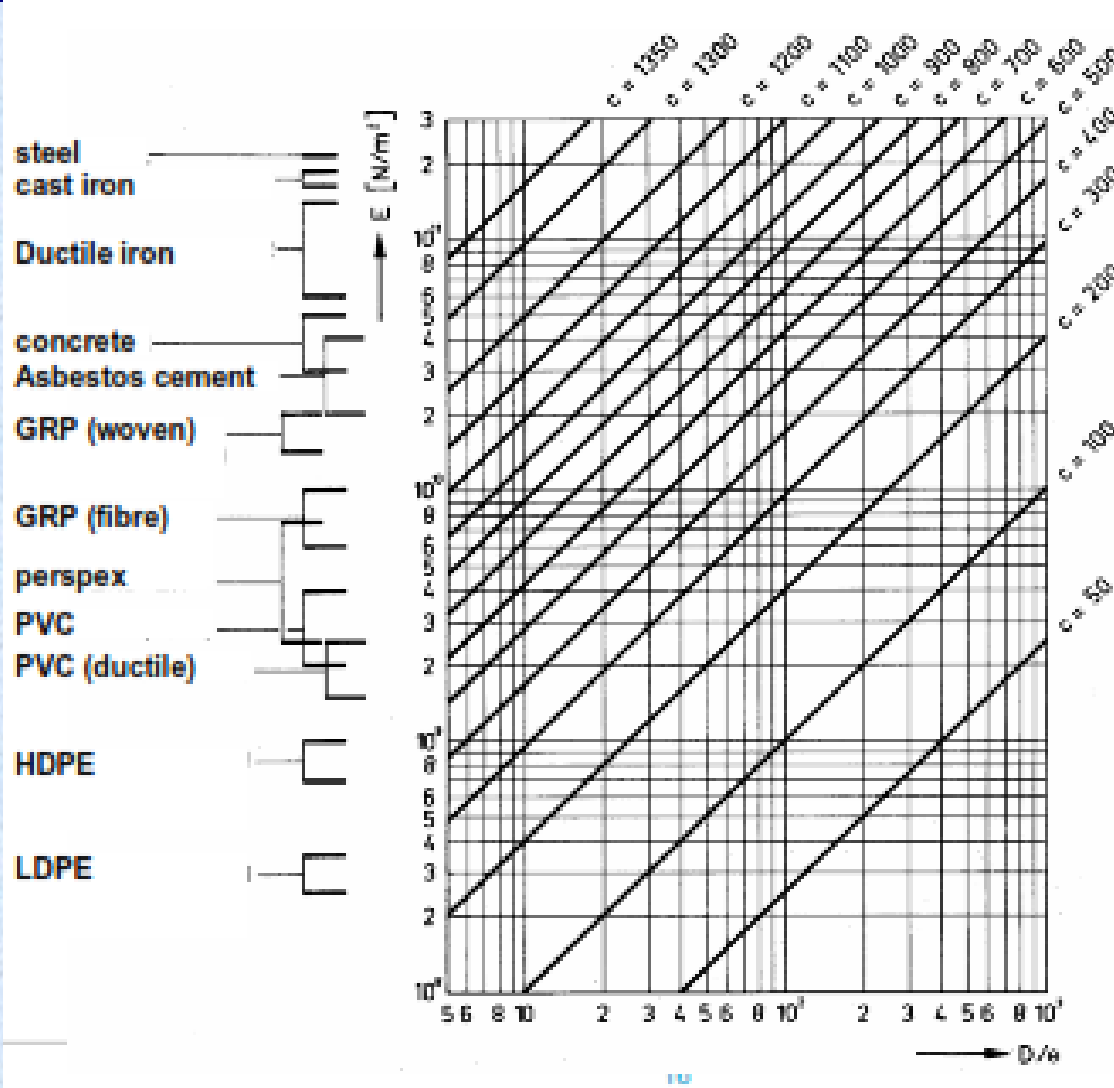
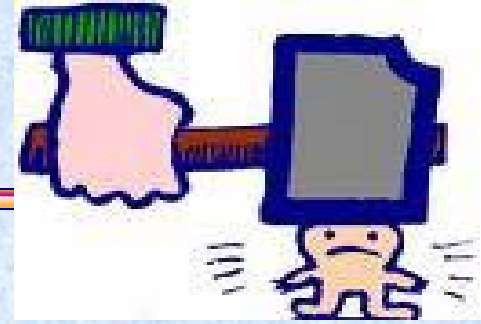


# Elastic Model



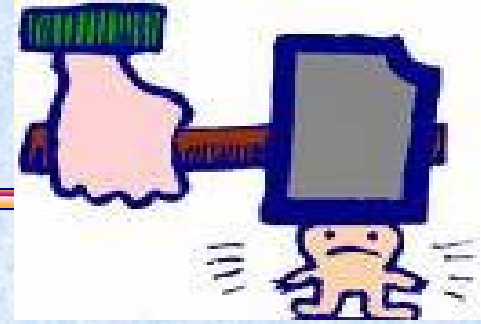


# Elastic Model





# A Comparison of the Models



$$\frac{\Delta p_{rigid}}{\Delta p_{elastic}} \propto \frac{L \frac{dV}{dt}}{(a)dV}$$

where  $\Delta p_{rigid}$  = change in pressure computed with rigid model

$\Delta p_{elastic}$  = change in pressure computed with elastic model

$dV/dt$  = fluid acceleration



# Application

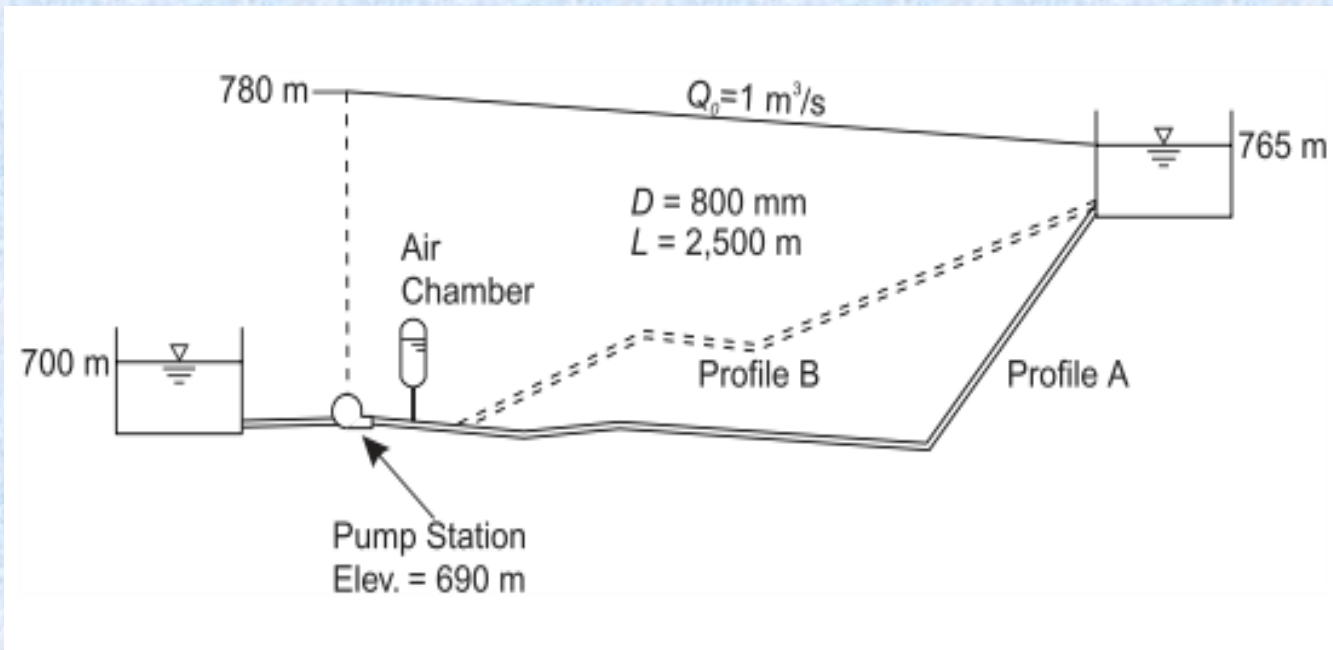
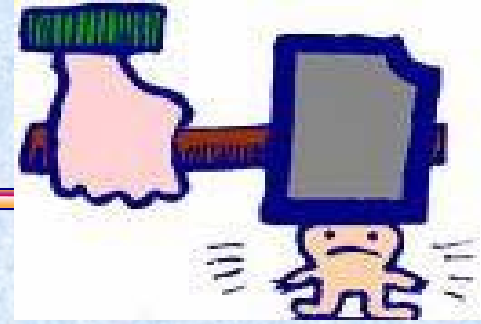


## □ Example

■ **Example – Analysis of a Piping System.** A pumping station located at an elevation of 690 m (2,263 ft) delivers 1 m<sup>3</sup>/s (35.3 ft<sup>3</sup>/s) of water from a suction well with a water surface elevation of 700 m (2,296 ft), as shown in Figure 13.15. The water is delivered through a check valve and 2,500 m (8,200 ft) of 800-mm (31-in.) pipe to a reservoir with a water surface elevation of 765 m (2,510 ft). The wave speed  $a$  is approximately 980 m/s (3,220 ft/s). The pump station includes a double suction pump that operates at 880 rpm and is driven by a 1,000 kW (1,341 HP) motor. The combined inertia of the pump and motor is approximately 150 kg-m<sup>2</sup> (3,562 lbm-ft<sup>2</sup>).



# Application



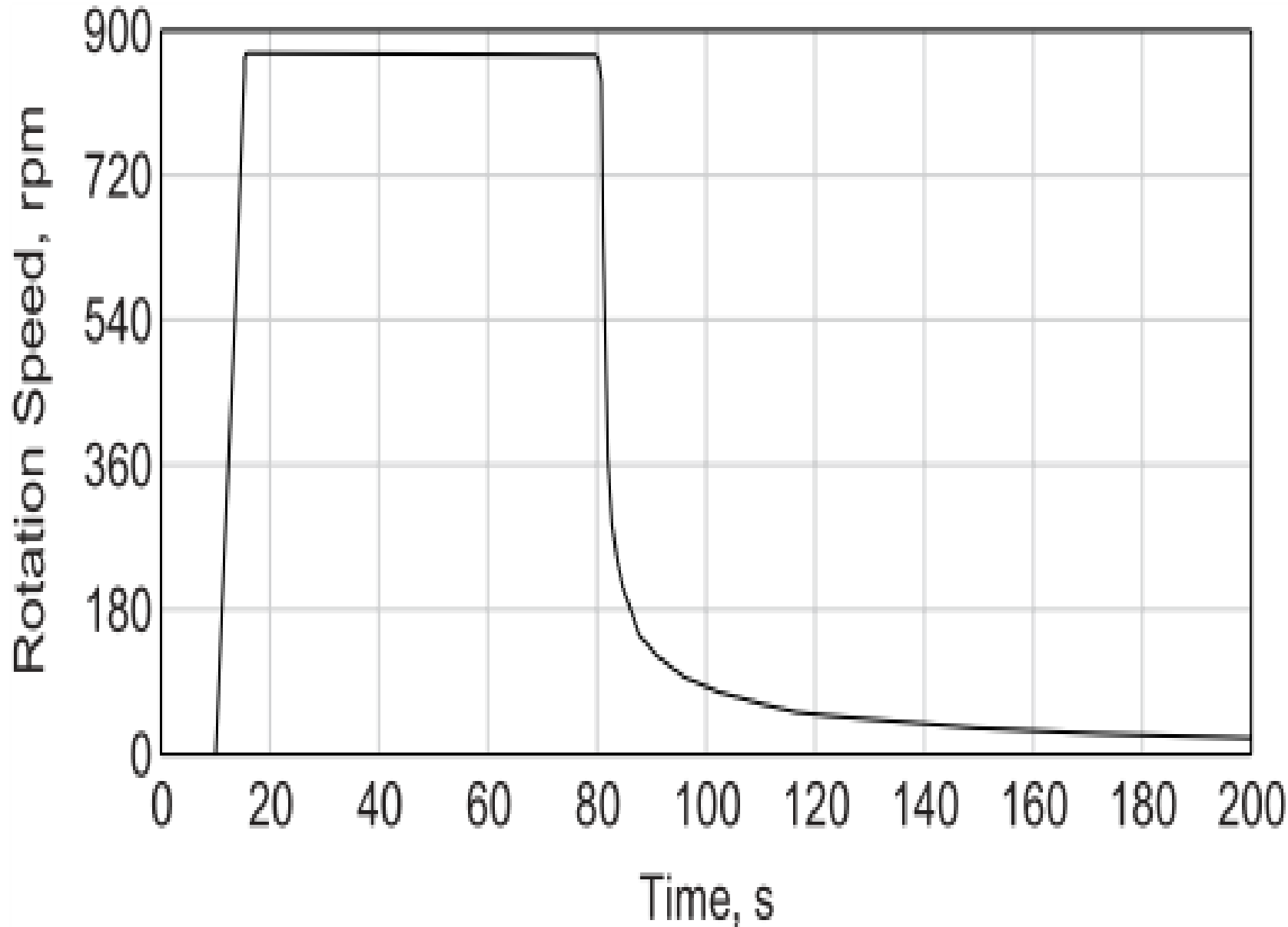




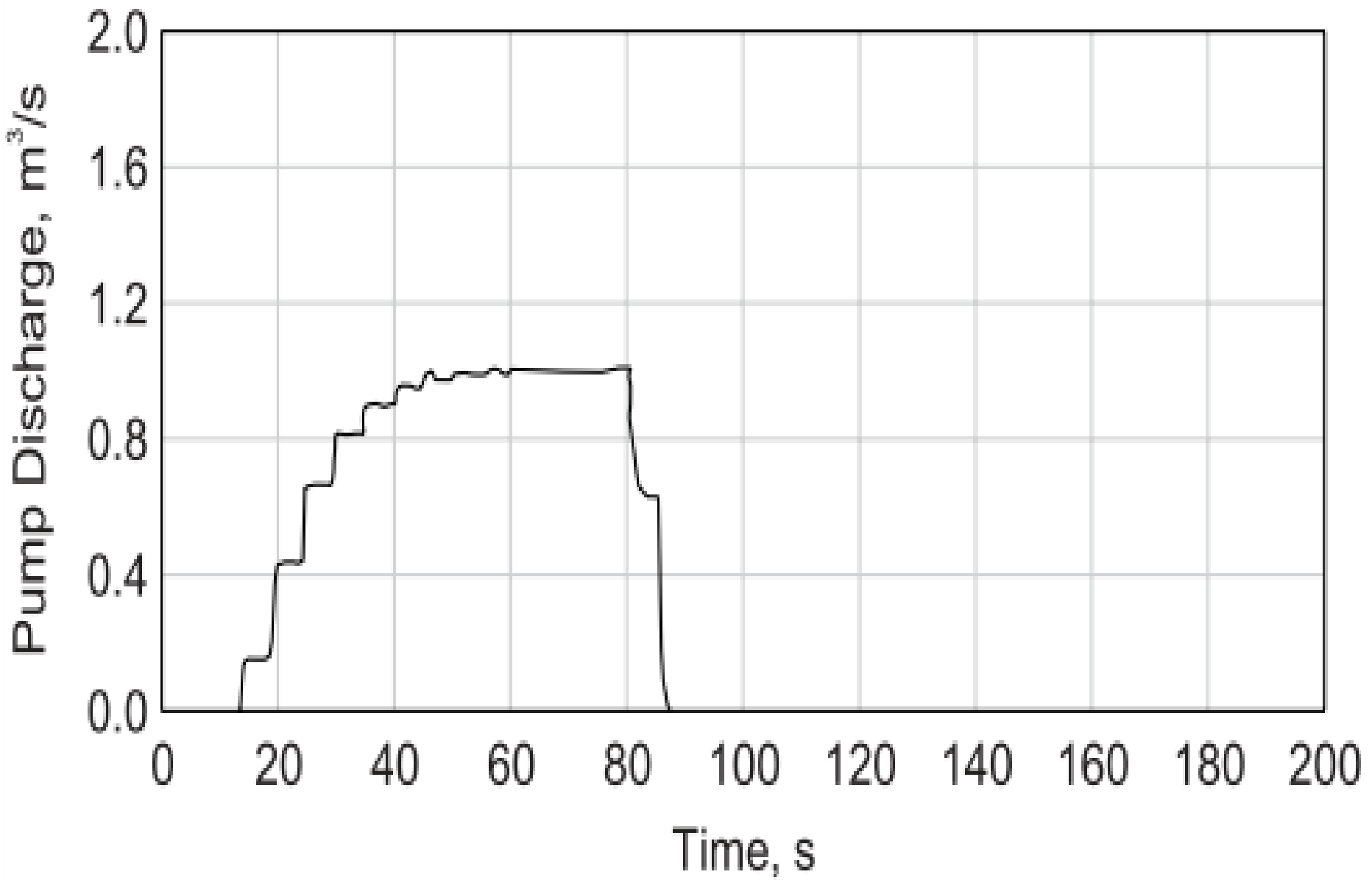
# Application



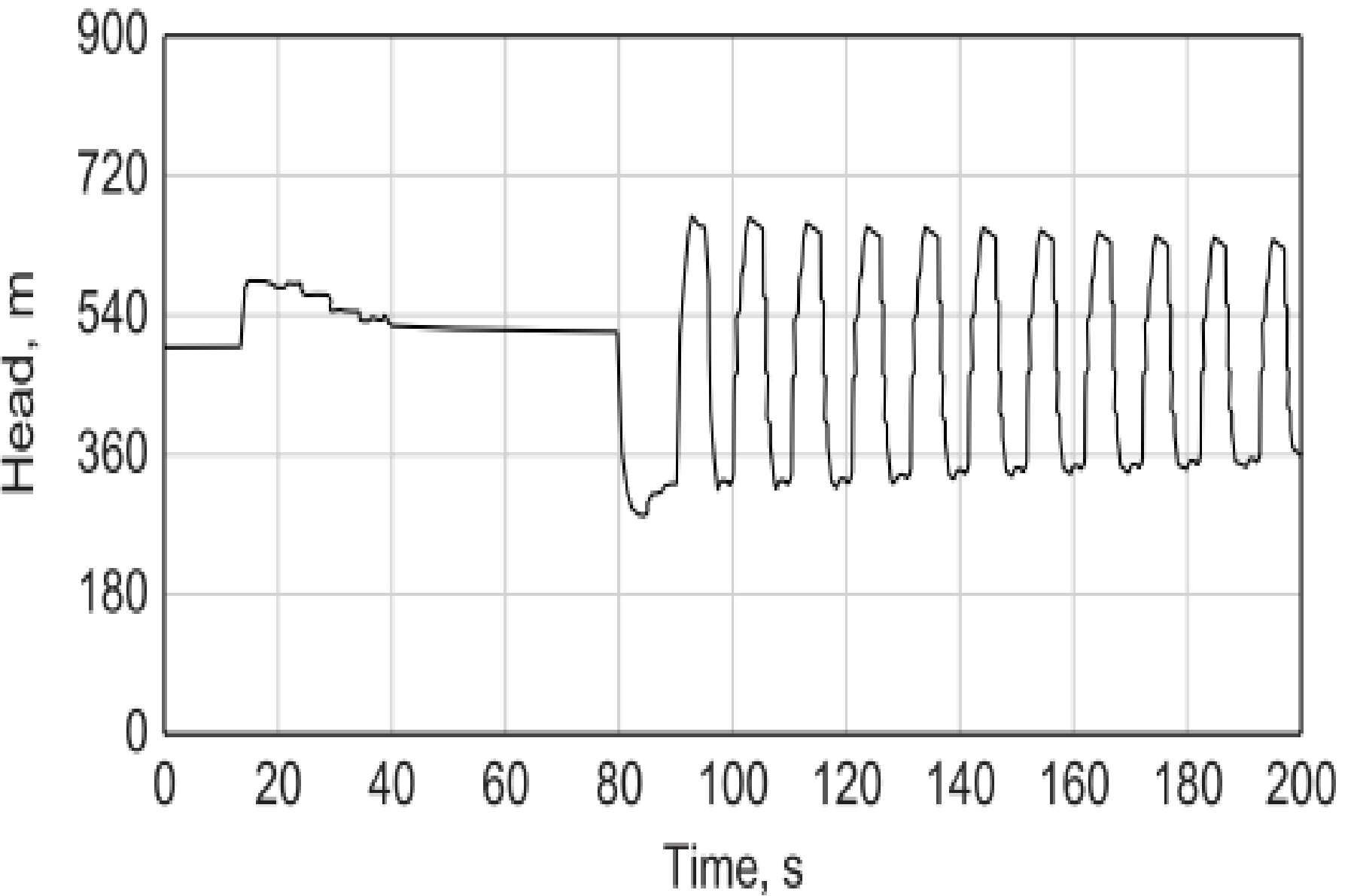
The pump is started at time  $t = 10$  seconds and takes approximately 4 seconds to ramp up to full speed [see Figure 13.16(a)]. A blow-off valve located at the pump discharge opens to relieve flow during pump start-up, and then gradually closes to direct water down the transmission main [Figure 13.16(b)]. At time  $t = 80$  seconds, a pump shutdown caused by a loss of electric power occurs. This incident is indicated by the abrupt drop-off in speed and flow in Figures 13.16(a) and (b). The shutdown is considered an emergency condition. Figure 13.16(c) shows the simulation results from a transient analysis computer program for the period including the pumping operations at time  $t = 10$  seconds (pump start) and  $t = 80$  seconds (pump failure).



**(a) Pump Rotation**



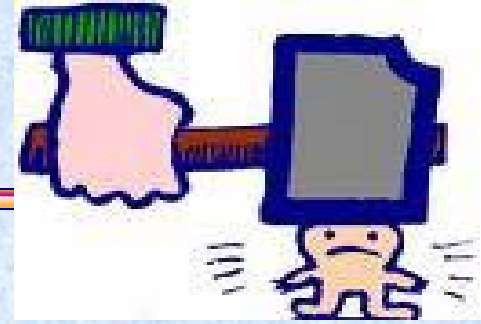
**(b) Pump Flow**



**(c) Heads in the Pump Discharge**



# Water Hammer- Mitigation



- Possible strategy's
  - Minimizing possibility of transient conditions during design
  - Install transient control devices



# Water Hammer- Mitigation



- The basis

$$\Delta p = \rho a \Delta V \text{ or } \Delta H = \frac{a}{g} \Delta V$$

$$dH = \pm \frac{a}{g} dV = \pm \frac{a}{gA} dQ = \pm B dQ$$



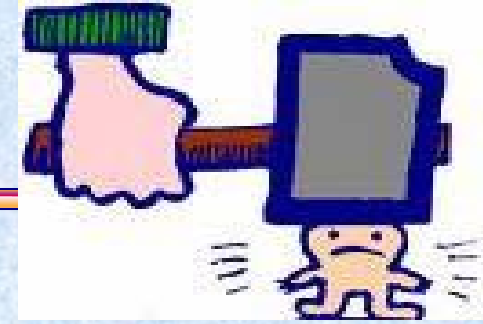
# Water Hammer- Mitigation Philosophy

- Philosophy
  - Reduce wave speed
  - Reduce rate of “ $\Delta v$ ”
  - Limit local pressure
  - Geometrical modification





# Water Hammer- Mitigation

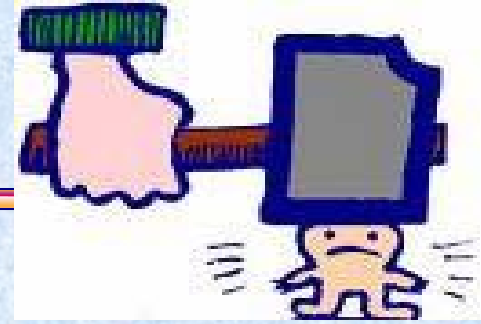


- ❑ System modifications
- ❑ Moderating the transient initiation event
- ❑ Emergency control procedures
- ❑ Anti- surge devices





# Water Hammer- Mitigation



- System modifications
  - Emergency flow control analysis
  - Route re-arrangement
  - Pipe thickness selection ( low head system)
  - Pipe material selection
  - Depth of overburden
  - Location and design of air valves
  - Pipe size



# Water Hammer- Mitigation



- Wave speed reduction methods
  - Determinants of wave speed
    - Elastic wall properties
    - Geometry
    - Liquid compressibility
    - Free gas content
  - Strategy
    - Bleeding in air
    - Pipe system configuration
    - Flexible hose



# Water Hammer- Mitigation

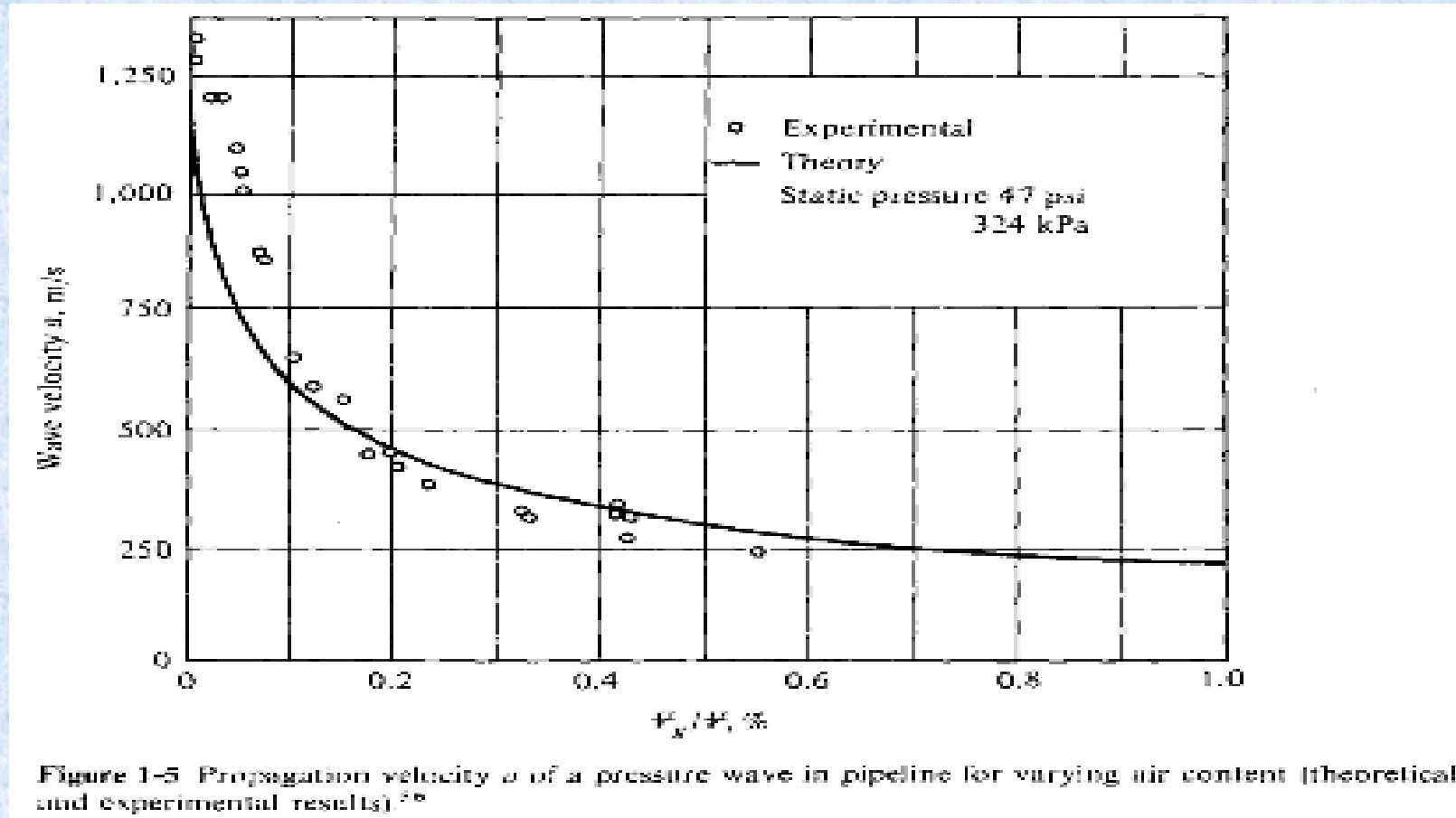


Figure 1-5 Propagation velocity  $a$  of a pressure wave in pipeline for varying air content (theoretical and experimental results) <sup>18</sup>



# Water Hammer- Mitigation



## □ Reduce rate of “ $\Delta V$ ”

- Air vessel
- Water tower
- One way tank
- Combined devices
- Soft start/stop or frequency driven pumps
- Slower valve manipulations
- Flywheel on pumps



# Water Hammer- Mitigation

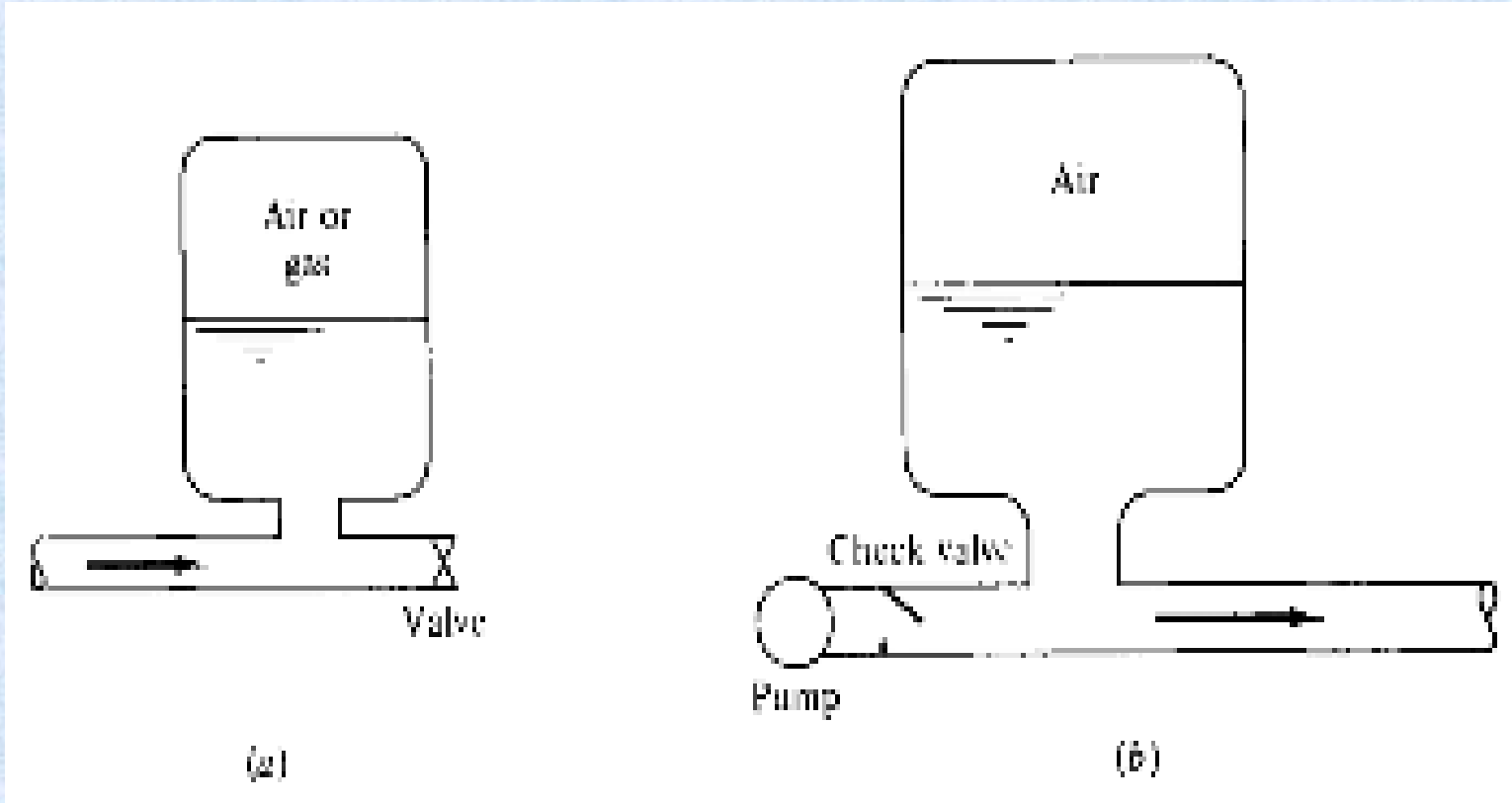
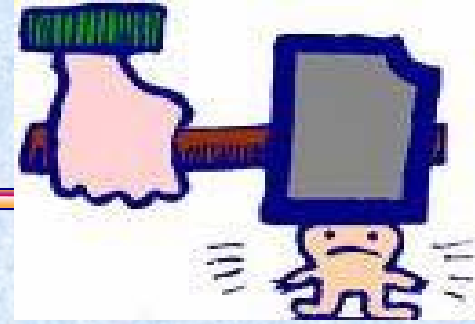


## □ Air Chamber

- Pressure control
- Container filled with system liquid and gas
- Pros
  - Function over wide range of pressure discharge combination
- Cons
  - Maintaining air volume
  - Biological contamination

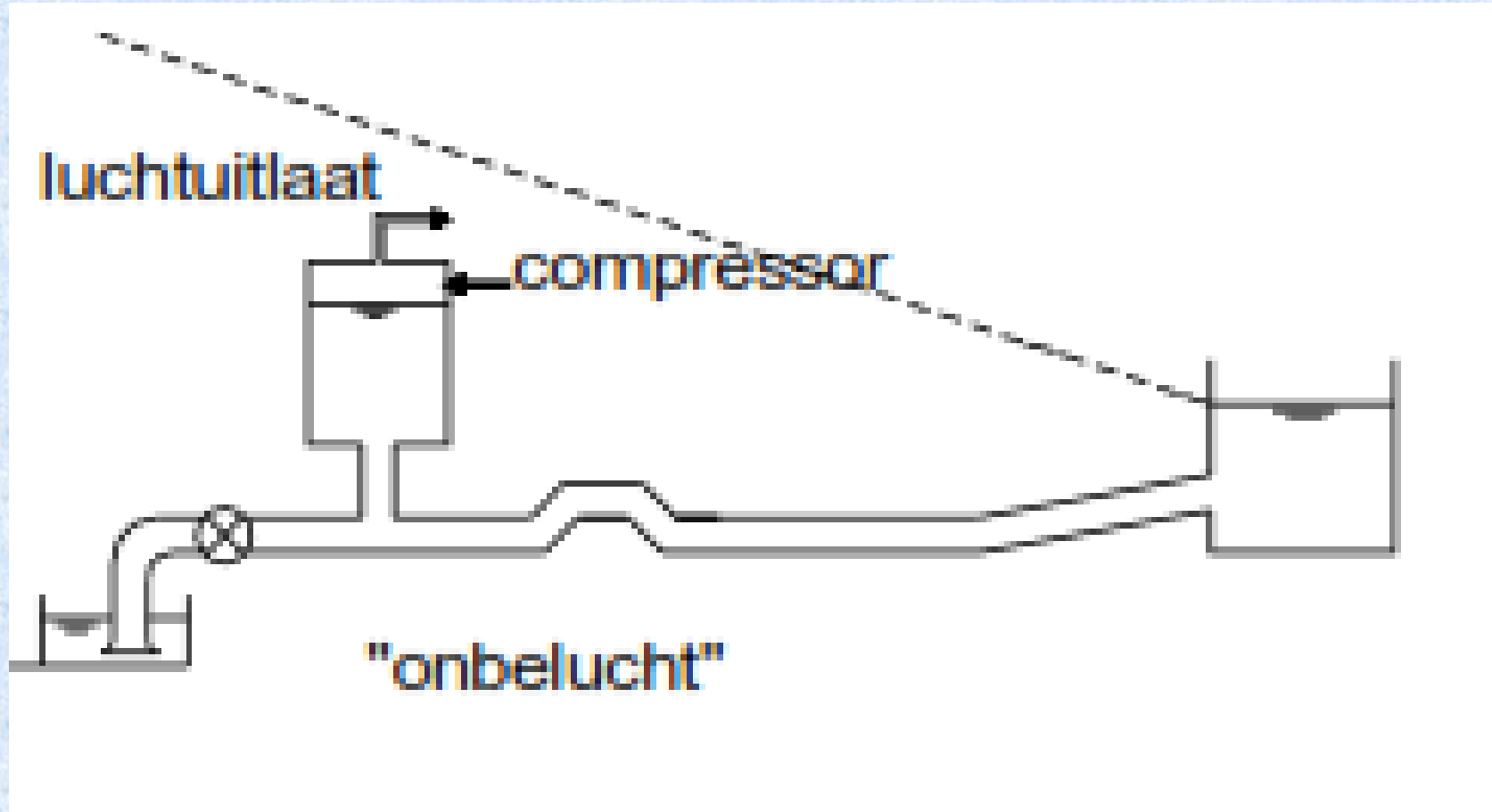
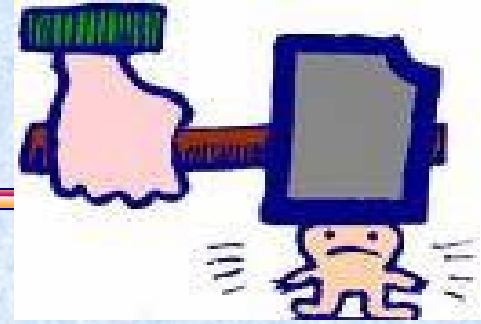


# Water Hammer- Mitigation



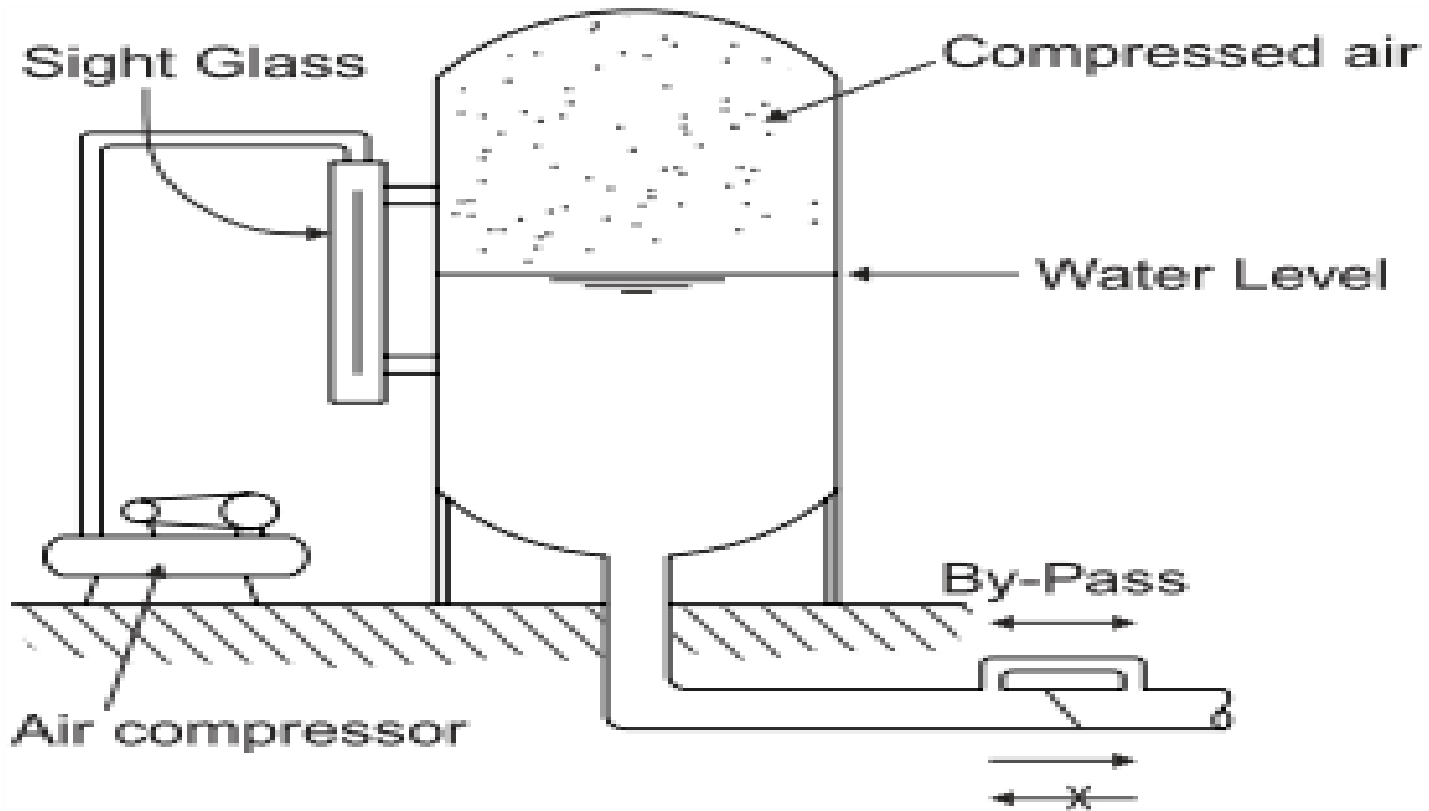
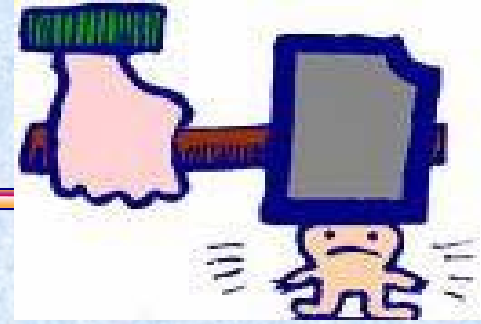


# Water Hammer- Mitigation





# Water Hammer- Mitigation

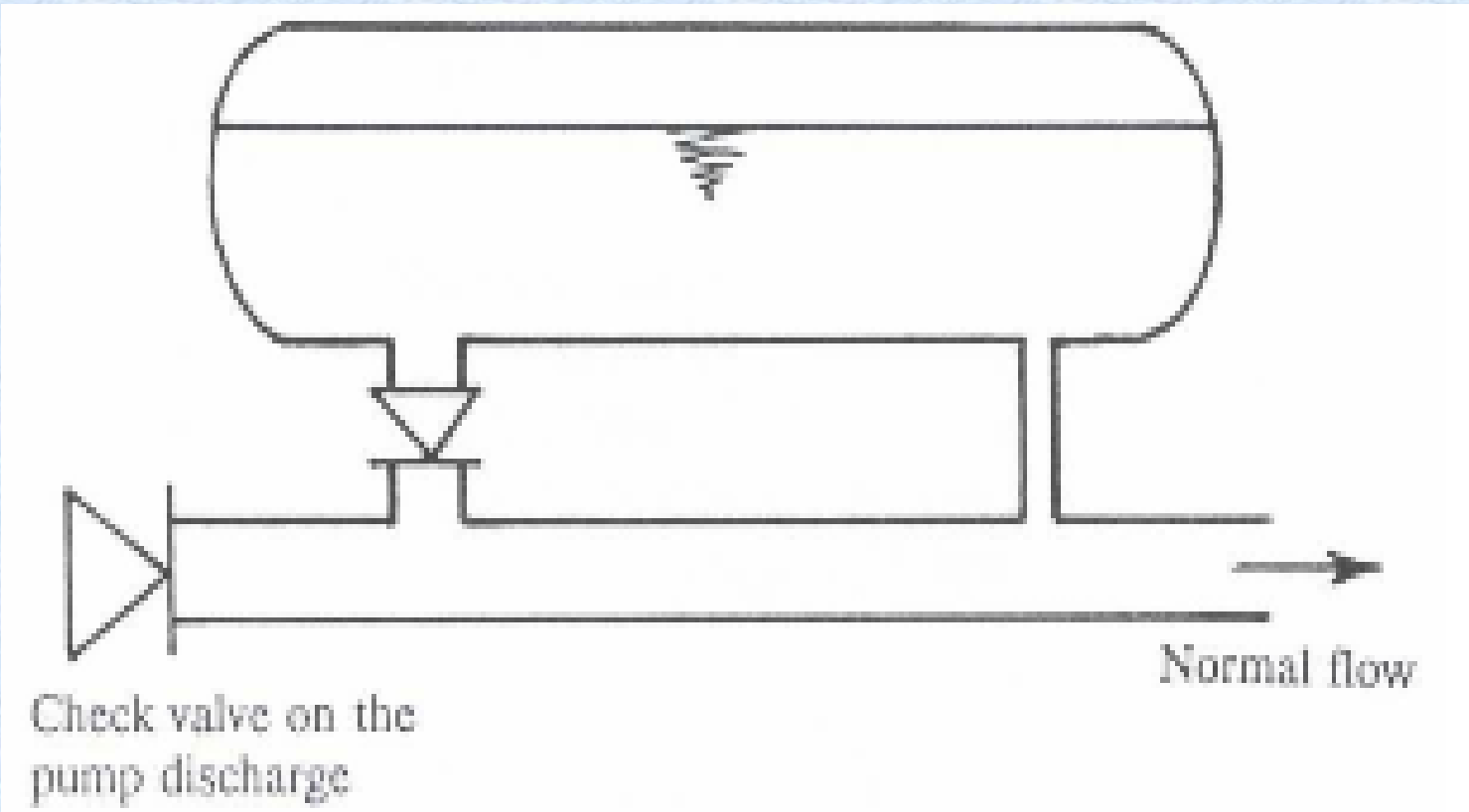


(a) Air Chamber



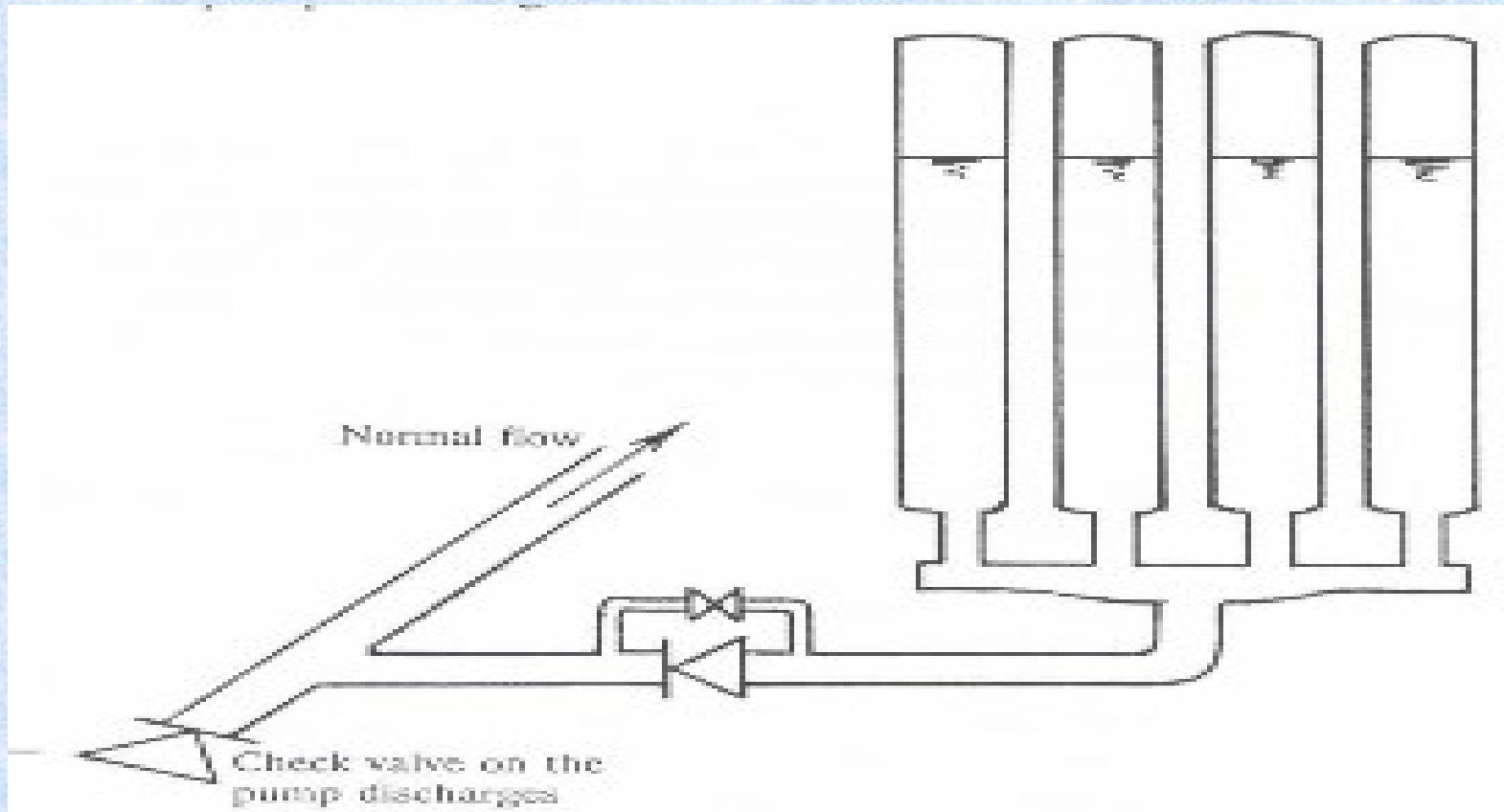
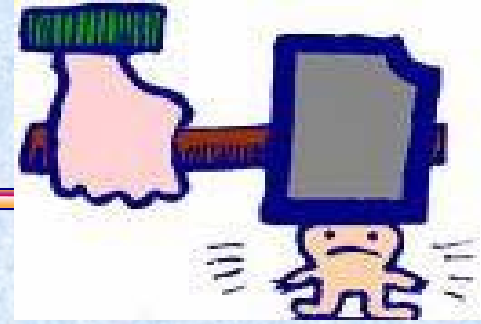


# Water Hammer- Mitigation



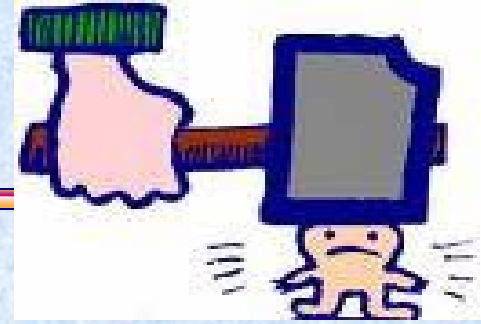


# Water Hammer- Mitigation

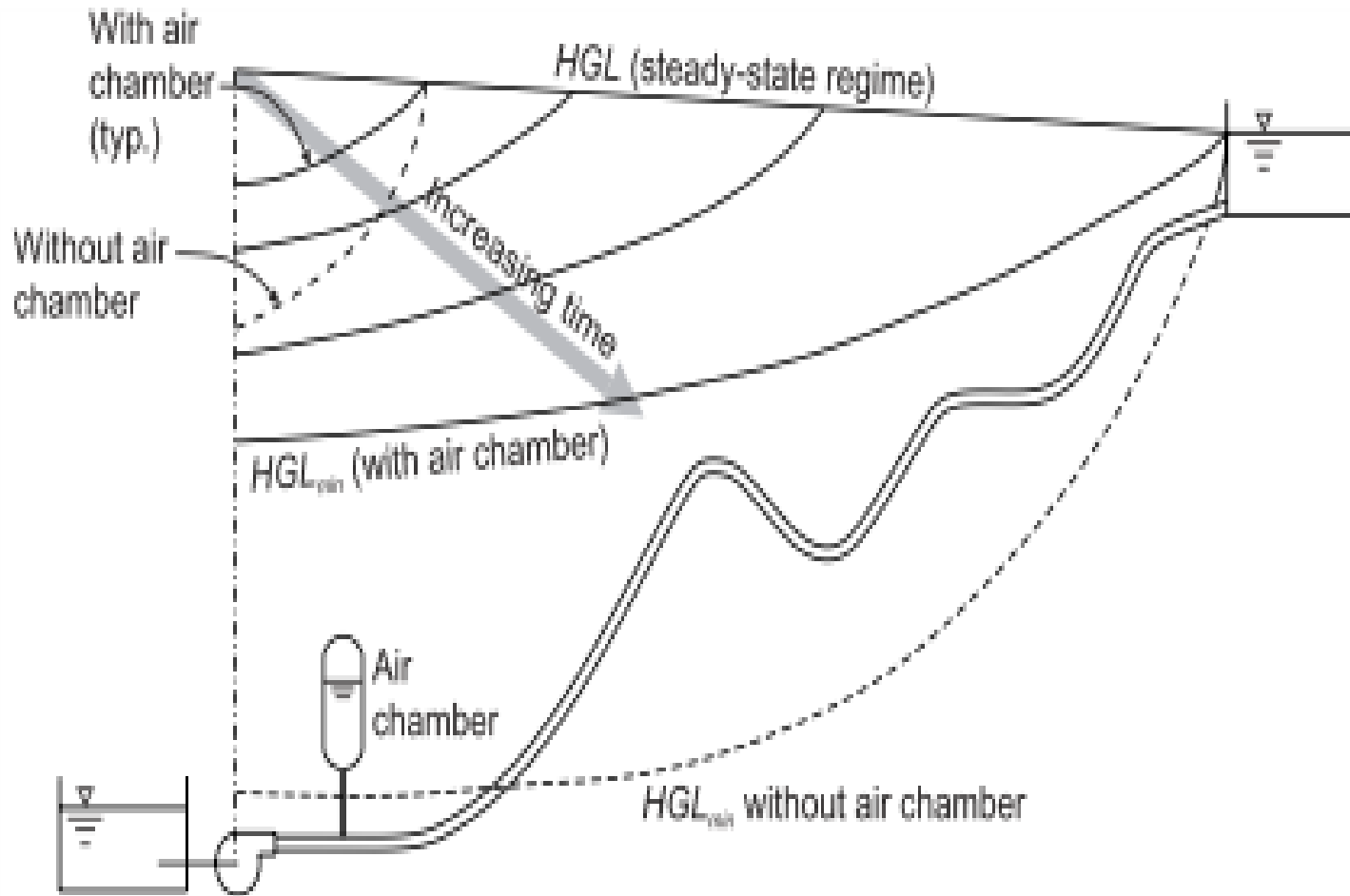




# Water Hammer- Mitigation



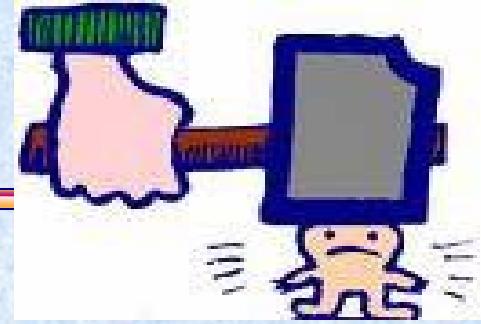
- Examples : Air Vessel



(a) Protection with Air Chamber



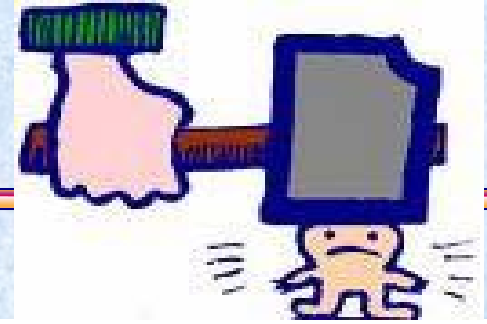
# Water Hammer- Mitigation



- Water Tower/Surge Tank :
  - Open tanks connected to the piping system.
  - Several forms of arrangement
    - Number
    - Arrangement
    - Nature of restriction
  - Pros :
    - Simple and reliable
    - Relatively large storage capacity



# Water Hammer- Mitigation



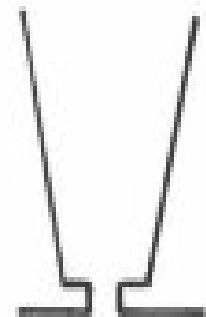
Simple



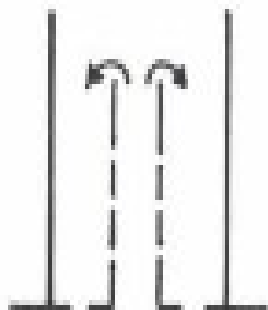
Multiple



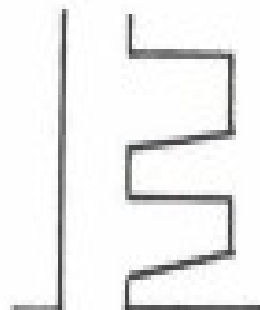
Orifice



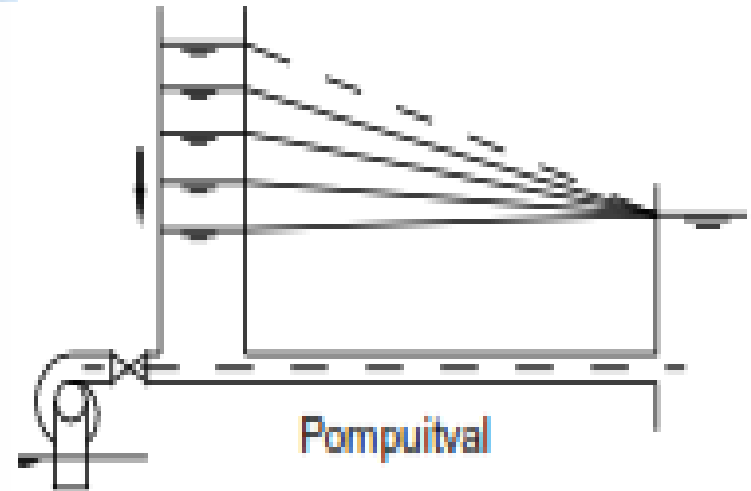
Tapered



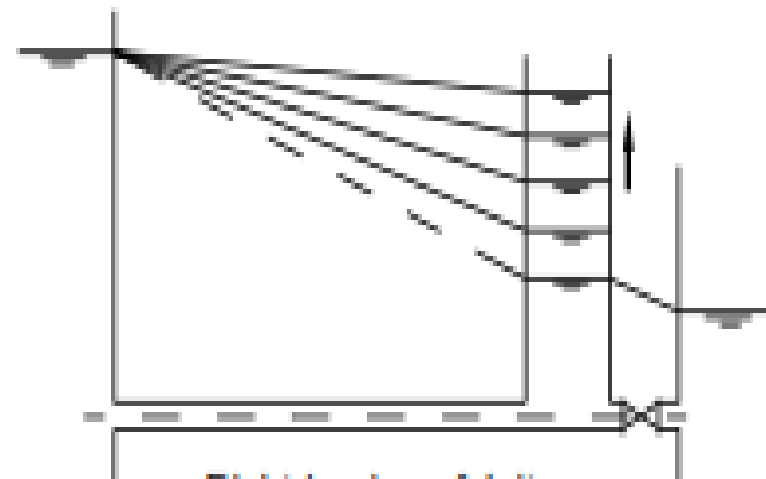
Differential



Galleried



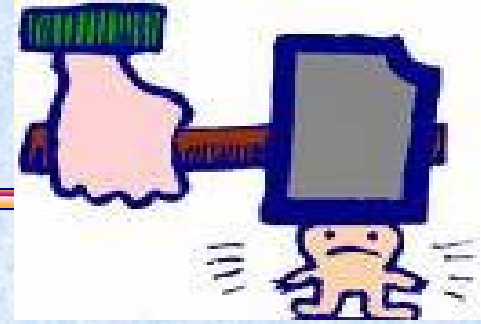
Pompuitval



Dichtdraaien afsluiter



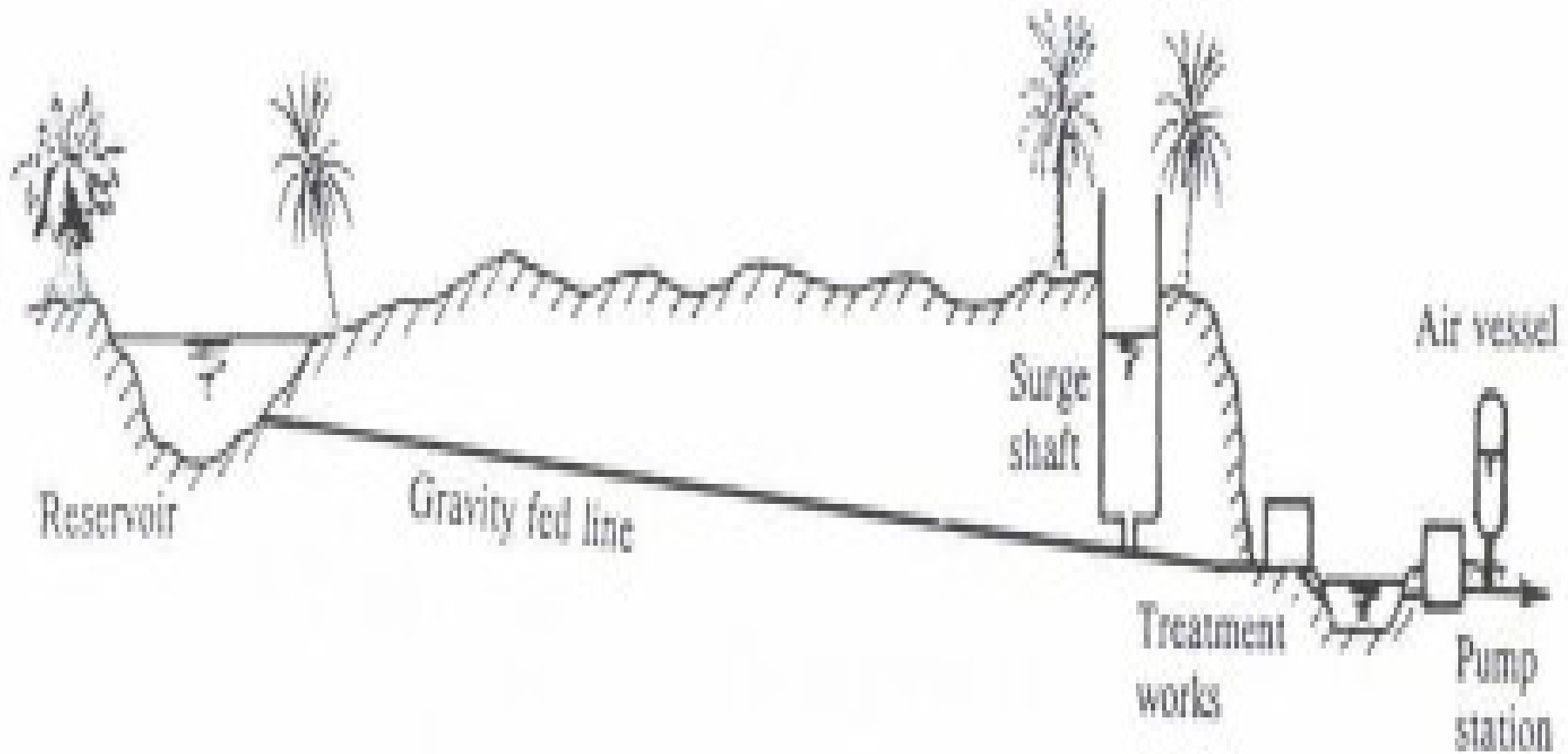
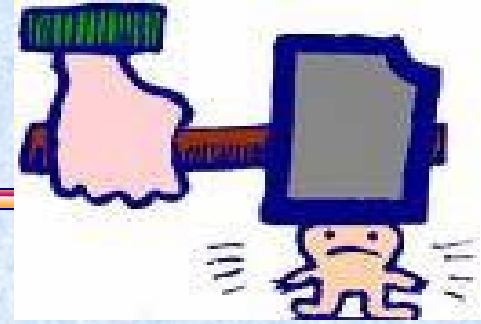
# Water Hammer- Mitigation



- Cons :
  - Application is limited
  - Rigidity
  - Odor problems
  - Water quality risk
  - Maintenance cost

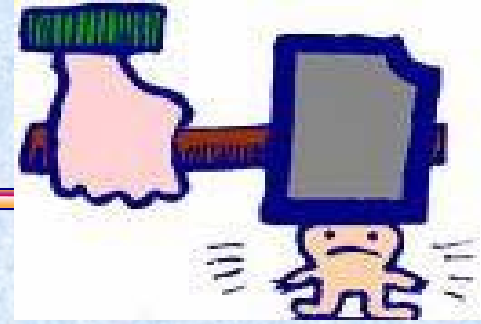


# Water Hammer- Mitigation





# Water Hammer- Mitigation

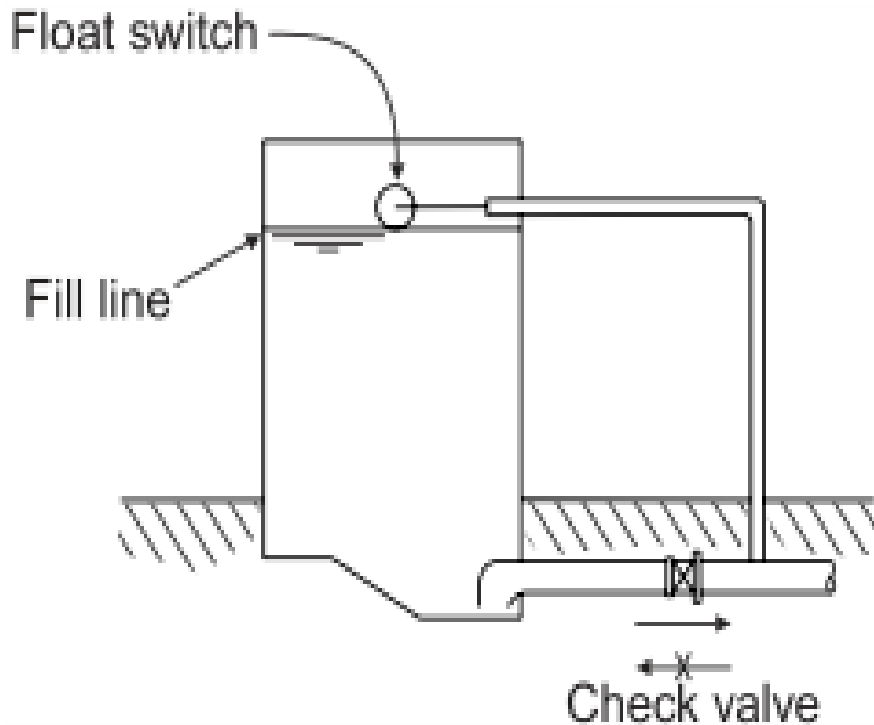
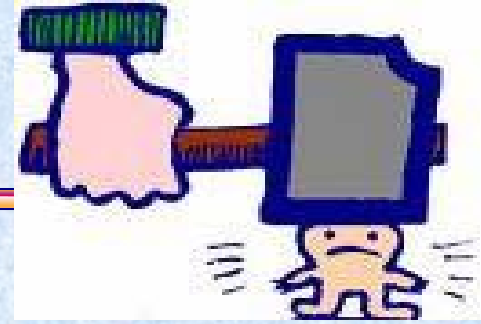


- ❑ One way tank
  - A storage vessel under atmospheric pressure
  - Low pressure control
  - Advantage
    - Effective under much lower height.





# Water Hammer- Mitigation





# Water Hammer- Mitigation



## □ By-Pass Line

### ■ Pros

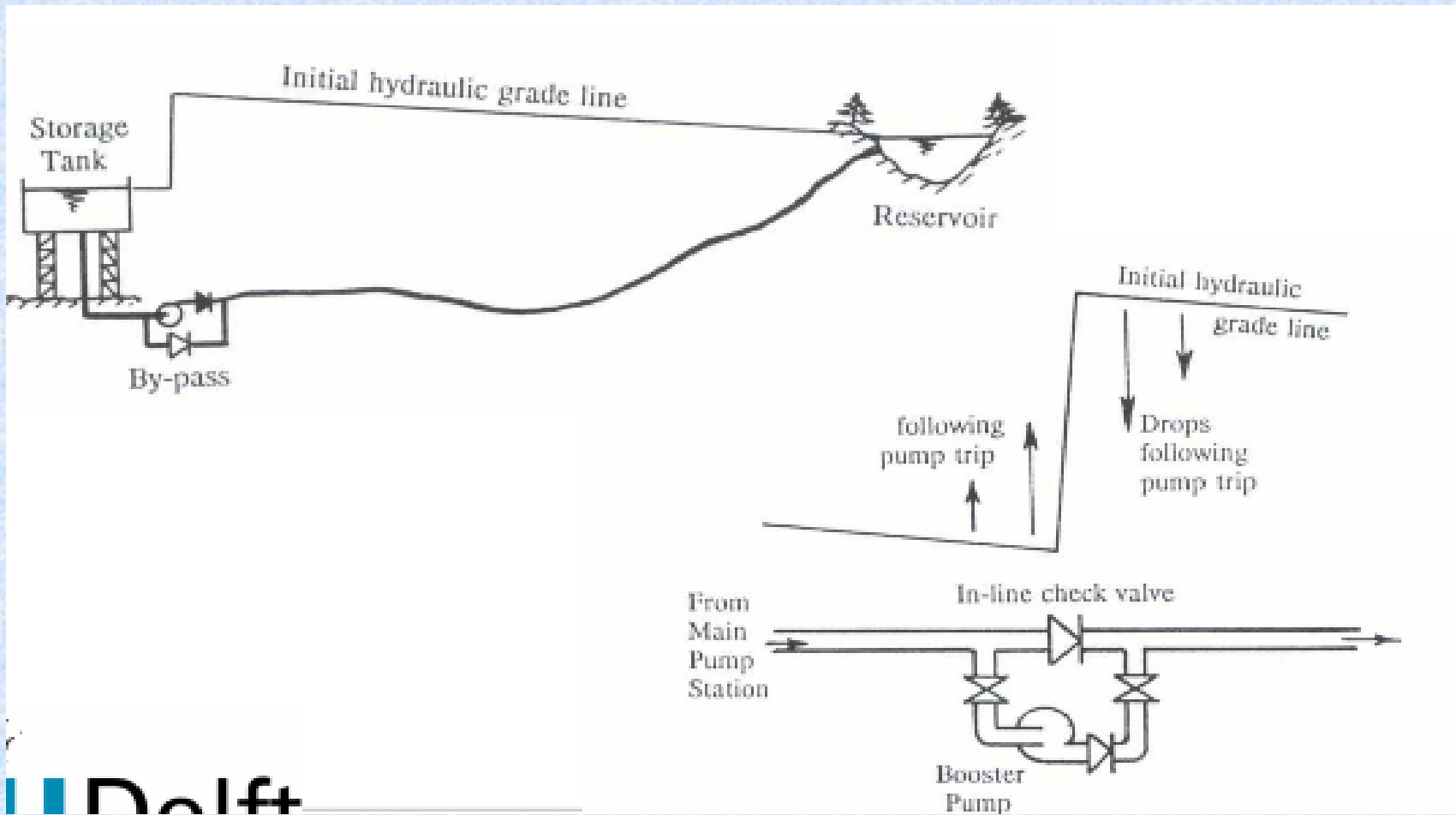
- No need for check valve

### ■ Cons

- Reservoir at sufficient level
- Late starting of action
- Limited application



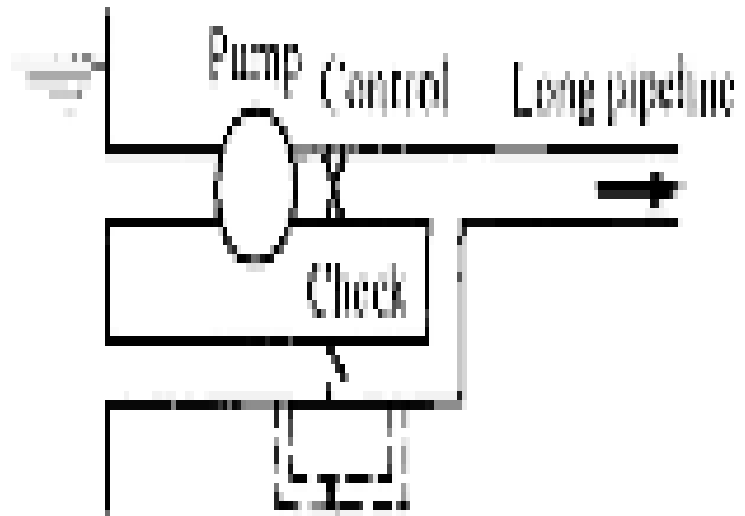
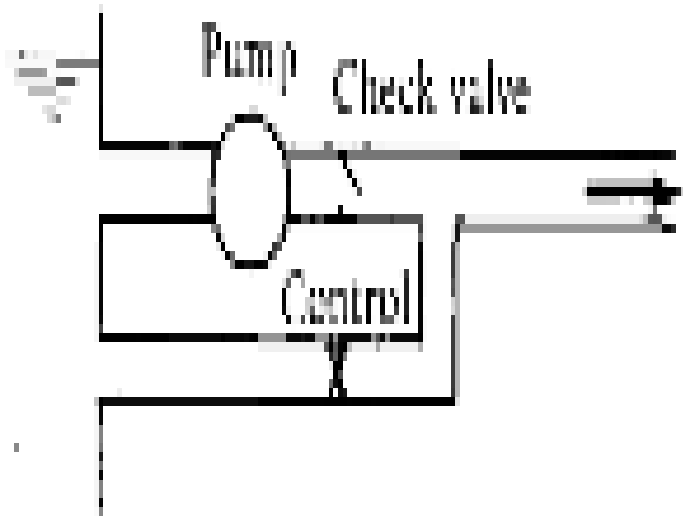
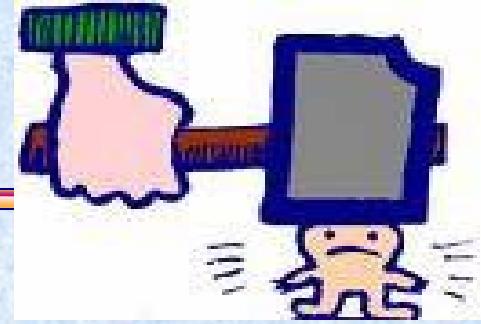
# Water Hammer- Mitigation



Delft

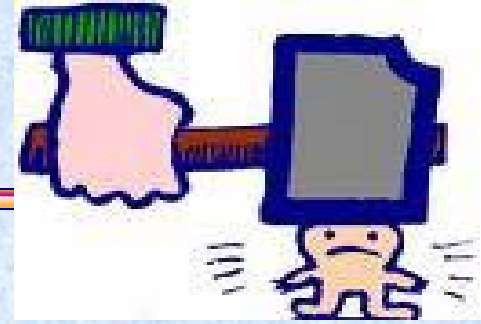


# Water Hammer- Mitigation





# Water Hammer- Mitigation

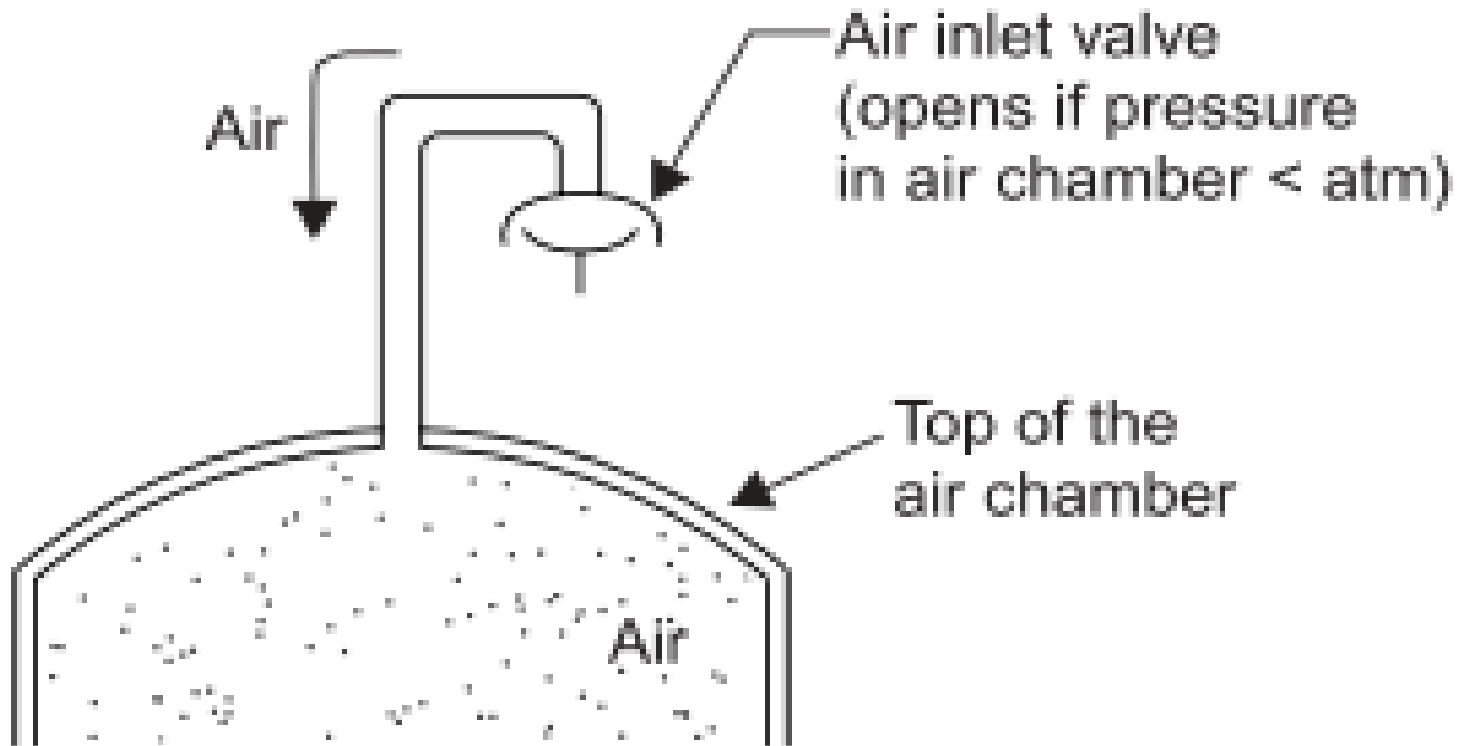
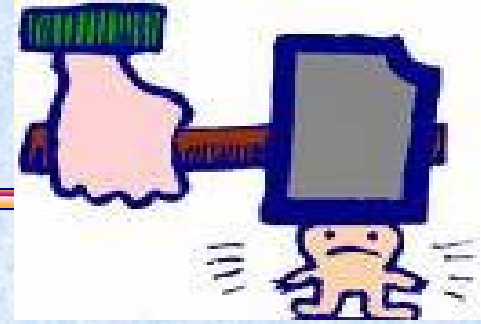


## ❑ Combined Devices

- Say an air chamber with an air inlet valve
- Pros
  - May lead to an optimum system design
  - Flexibility to operate in both extremes
- Cons
  - Special check valve arrangement
  - Special design requirements
  - Temperature sensitivity

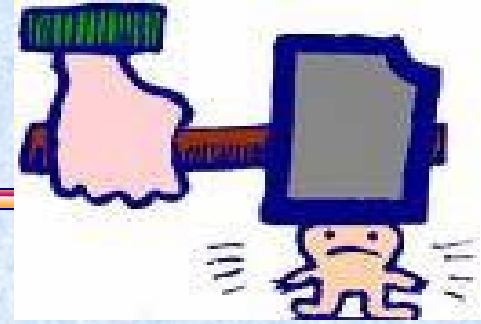


# Water Hammer- Mitigation





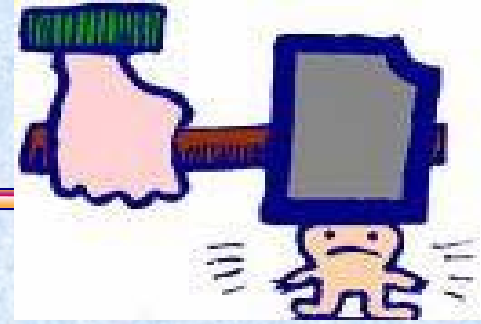
# Water Hammer- Mitigation



- ❑ Soft – starters/FO pumps
  - Pros
    - Beneficial during normal operation
  - Cons
    - Not applicable in power failure



# Water Hammer- Mitigation

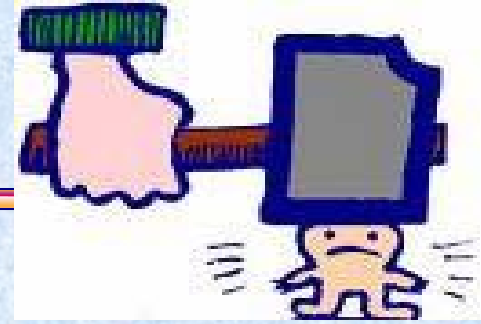


- ❑ Slower valve manipulation
  - Pros
    - No expensive anti-surge devices required
  - Cons
    - Manipulations must be slower than several pipe periods
    - Pipeline can not be blocked or opened quickly





# Water Hammer- Mitigation



## □ Flywheel

### ■ Pro

- Cheap construction
- Gradual check valve closure
- Limited maintenance

### ■ Cons

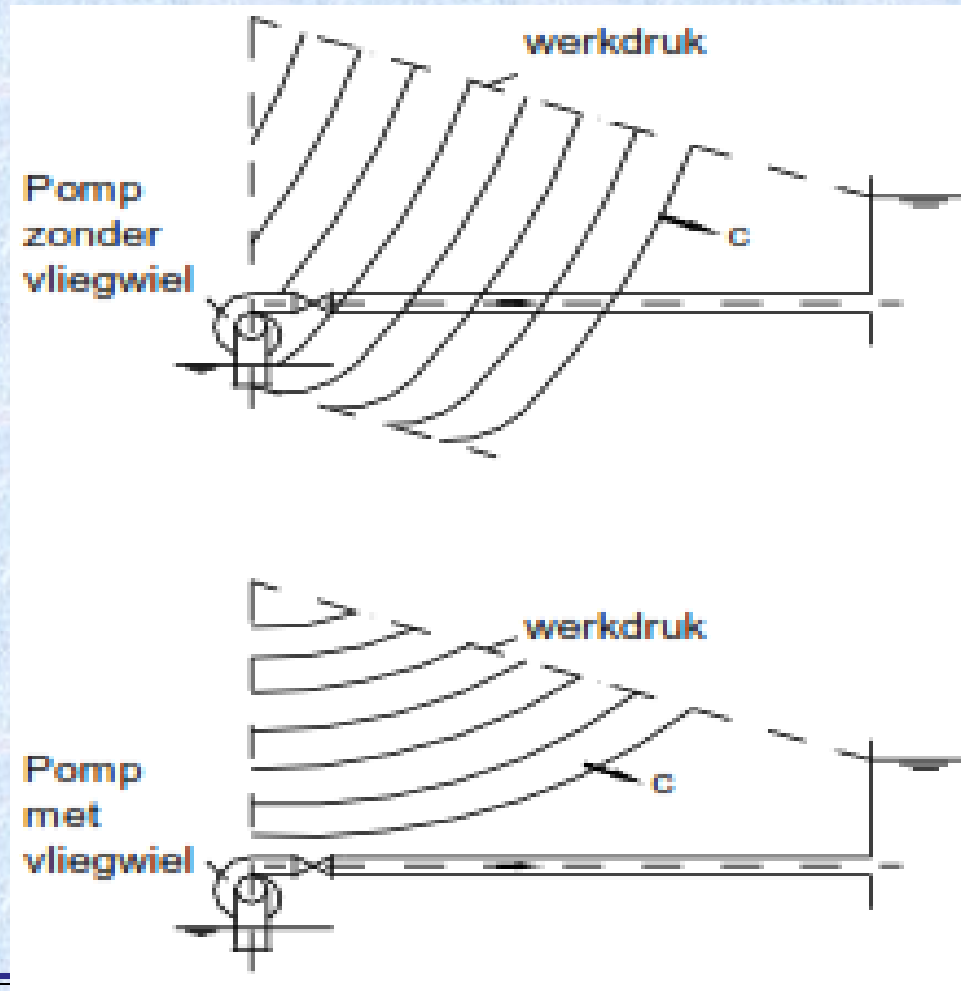
- Effect is limited to several km
- Pump motor must be large enough to start the flywheel
- No effect if impeller blocks



# Water Hammer- Mitigation

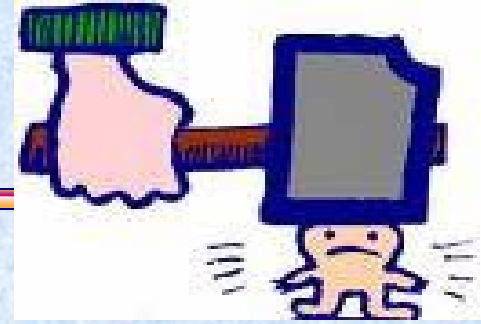


- Pump start costs more energy. Only economically feasible for pumps that run continuously on fixed speed





# Water Hammer- Mitigation



## □ Limit Pressure

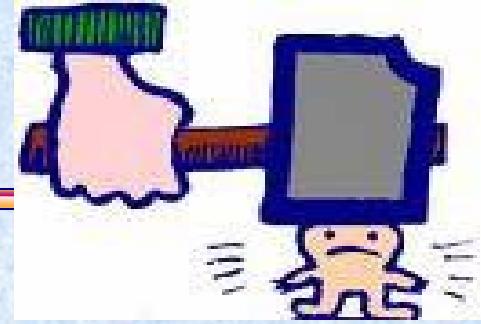
- Very localized

- Include :

- Pressure relief valve (PRV)/Safety valve
- Air valve/vent/vacuum breaker



# Water Hammer- Mitigation



## □ Pressure relief valve

### ■ Pro

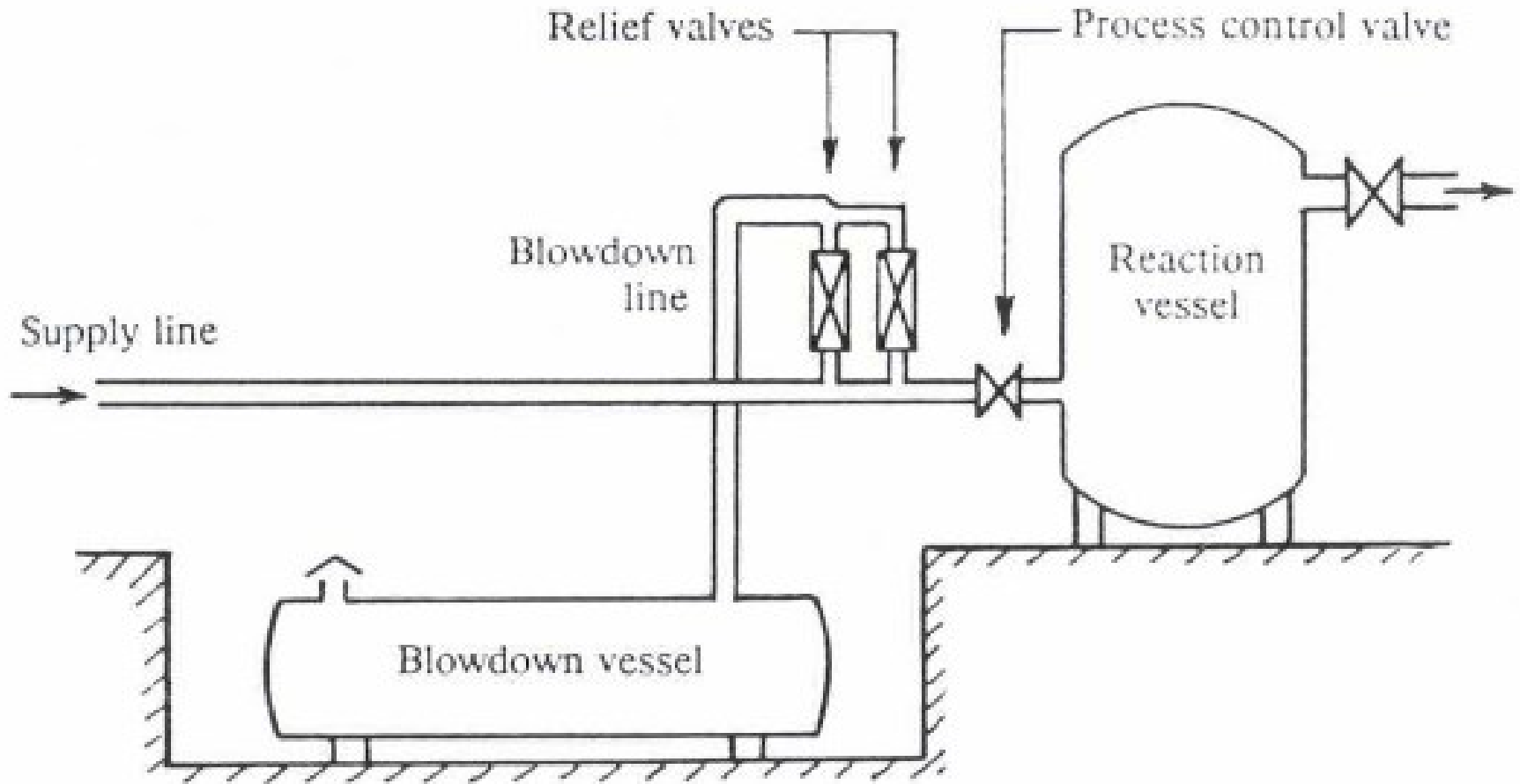
- Pressure is limited locally

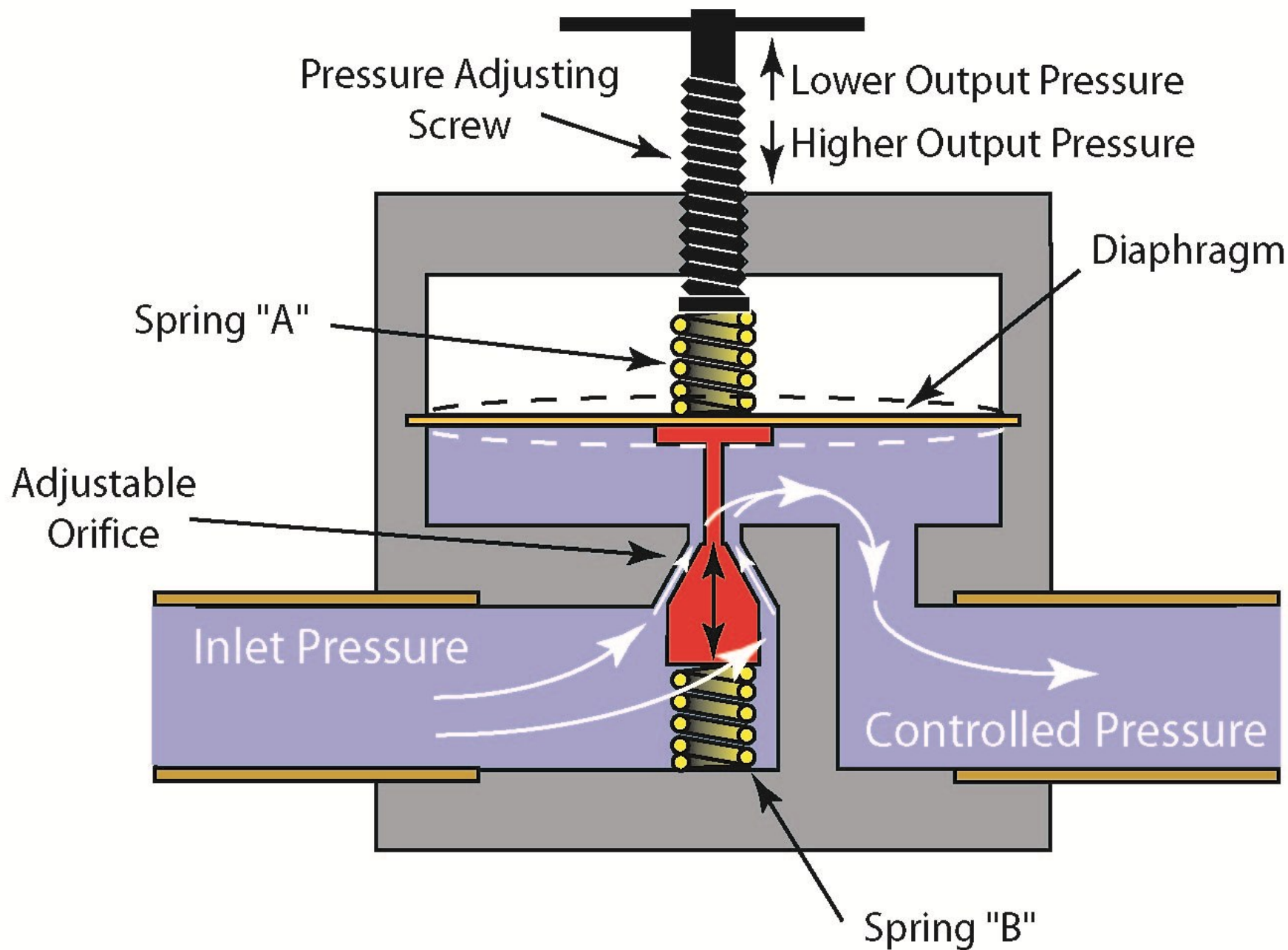
### ■ Cons

- Periodic maintenance required
- Relief lines to dump ejected liquids
- Risk of hammering PRV, if PRV capacity is not well sized



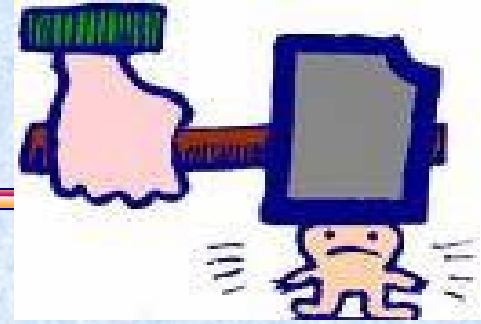
# Water Hammer- Mitigation







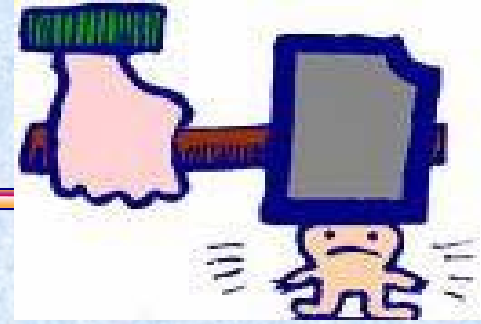
# Water Hammer- Mitigation



- Damper/ accumulator
  - Gas pocket separated by a membrane
  - Pro
    - No direct contact with the liquid
    - Gas pocket does not dissolve
    - Set pressure provides flexibility
  - Cons
    - Volume limited
    - Activated only after set pressure is exceeded



# Water Hammer- Mitigation



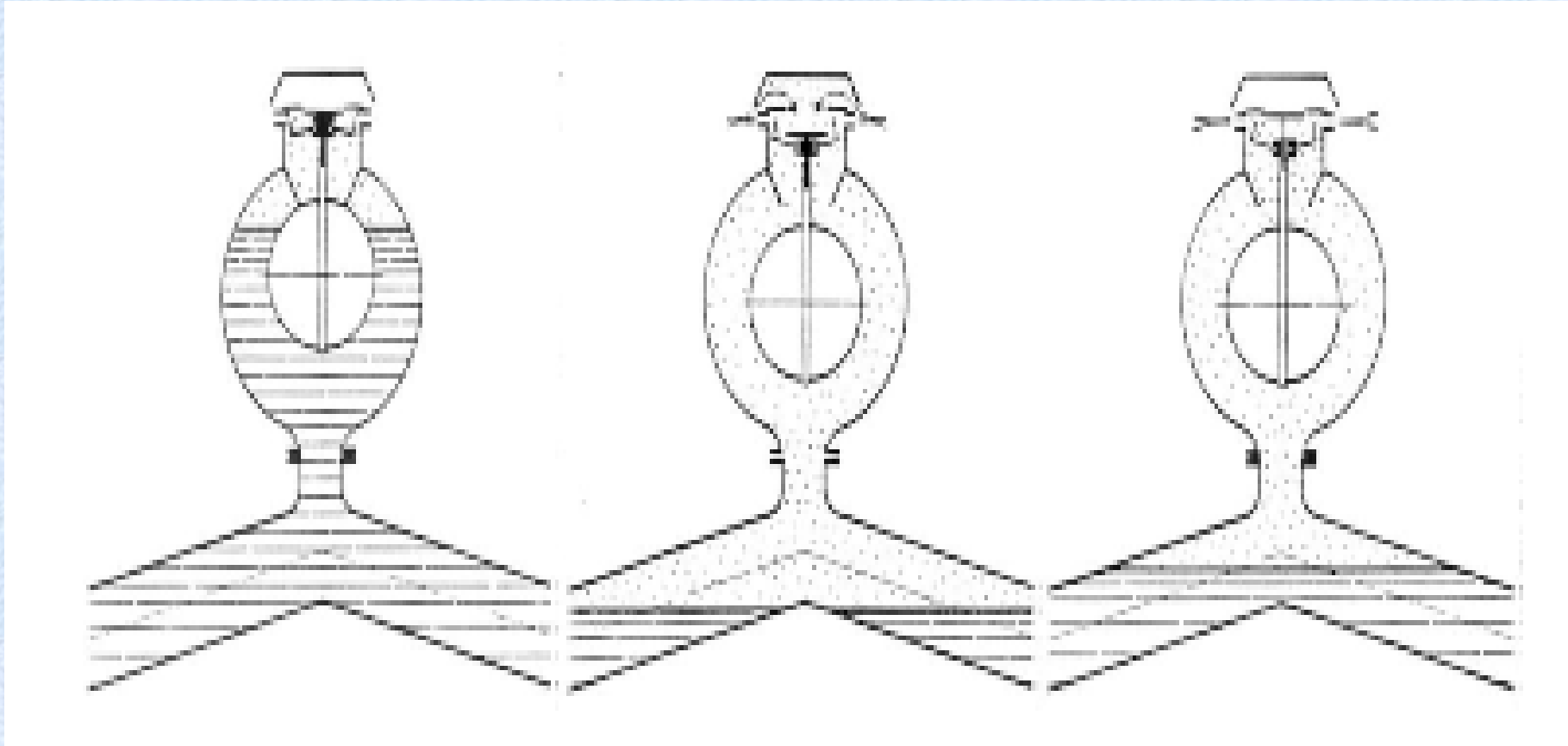
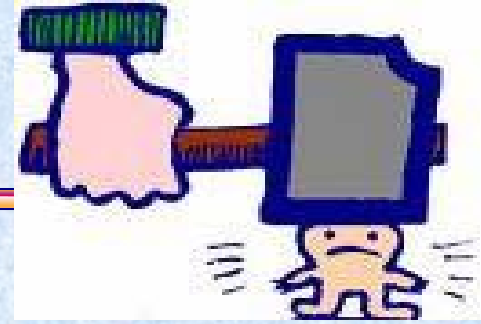
## □ Air Valve

- Control high pressure transients
- Pro
  - Limit pressure locally
- Cons
  - All incoming air should be released afterwards
  - Accuracy in installation and location
  - Vulnerable to fouling and blocking ( i.e. need periodic maintenance)



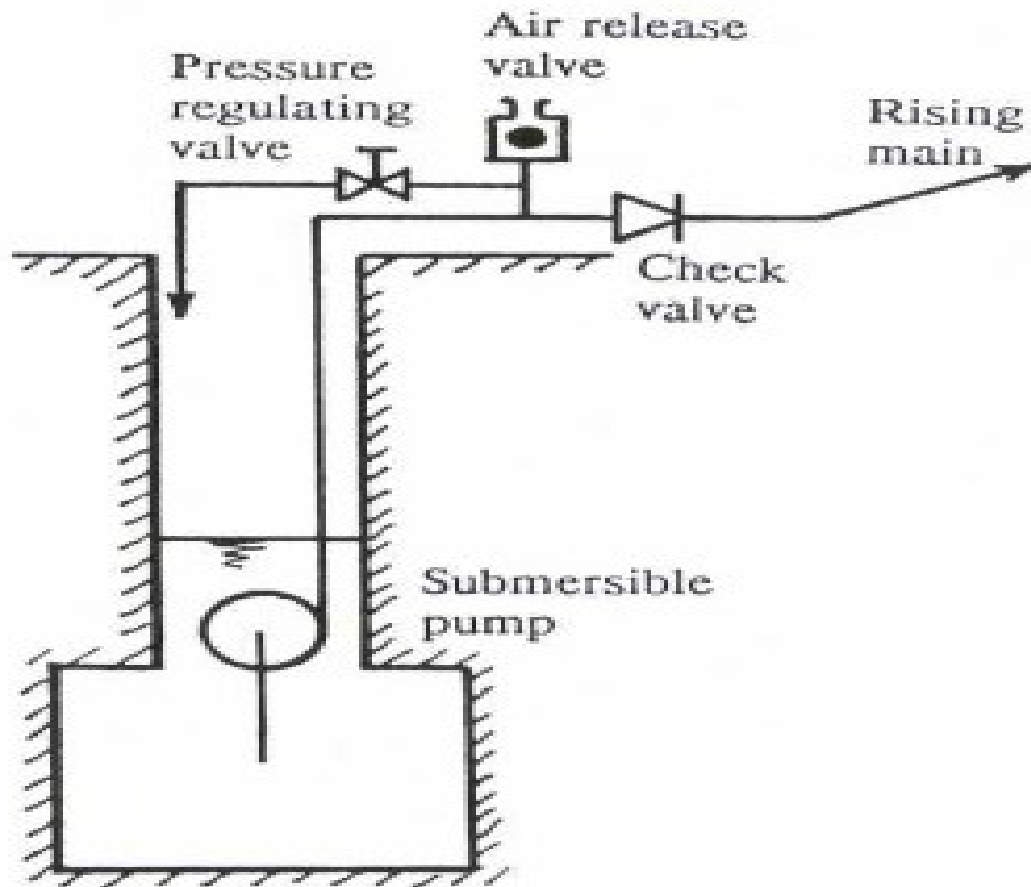
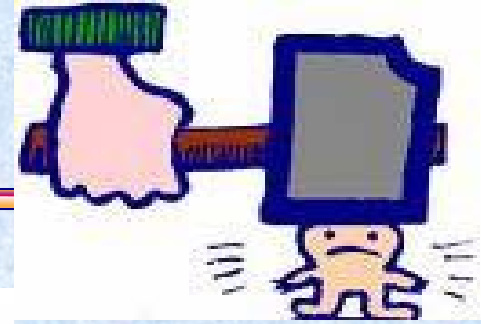


# Water Hammer- Mitigation





# Water Hammer- Mitigation





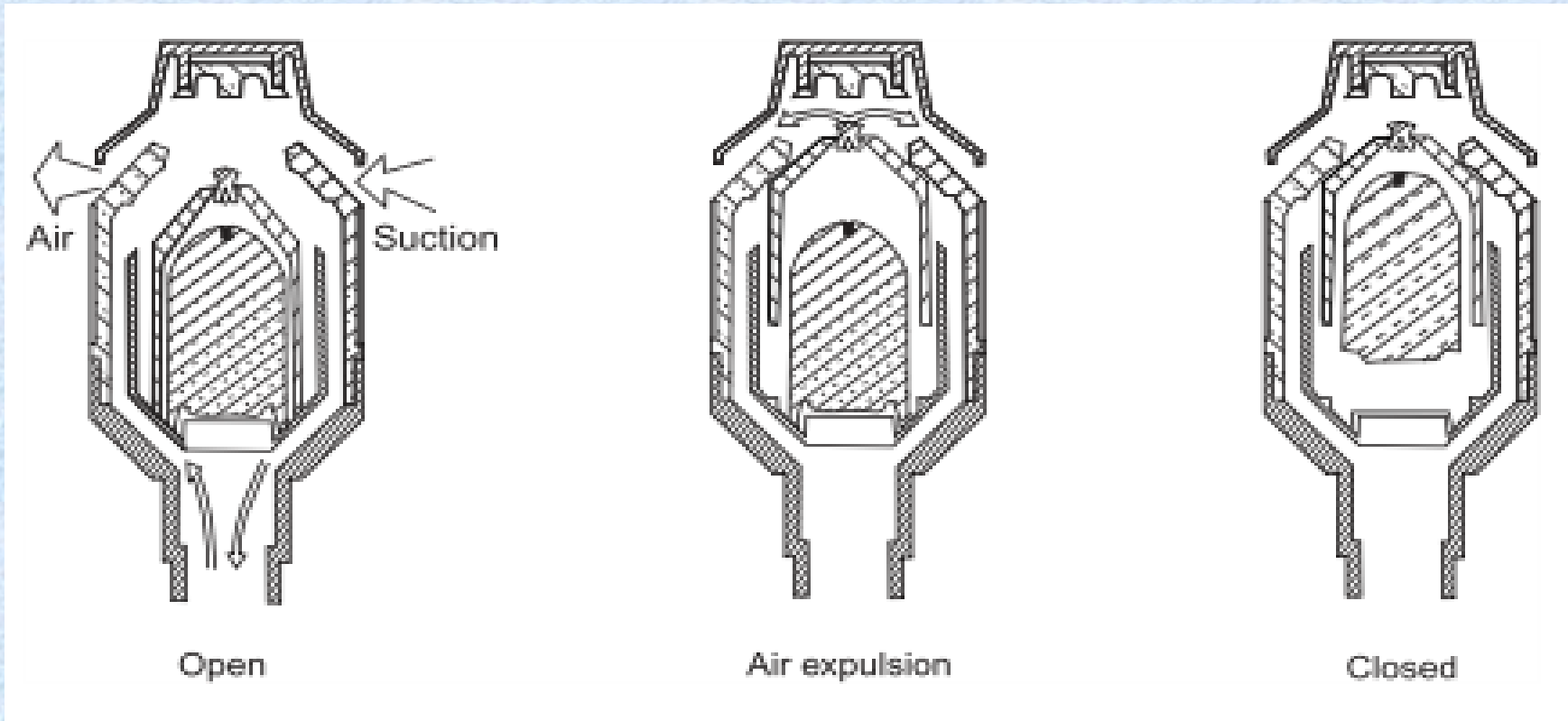
# Water Hammer- Mitigation



- ❑ More effective when high pressure transients occur quickly.
- ❑ Air Inlet Valves
  - Located at high points
  - Purpose – control
    - Vacuum condition
    - Potential column separation
  - Modus –operandi
    - Slow air removal
    - Adequate time

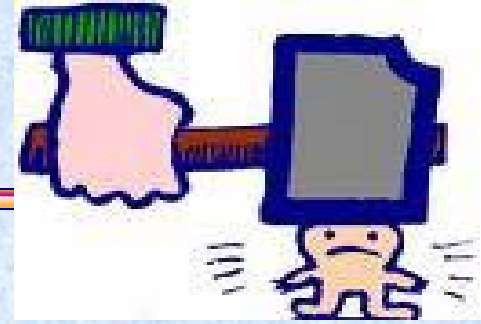


# Water Hammer- Mitigation





# Water Hammer- Mitigation



## □ Feed Tank

### ■ Pro

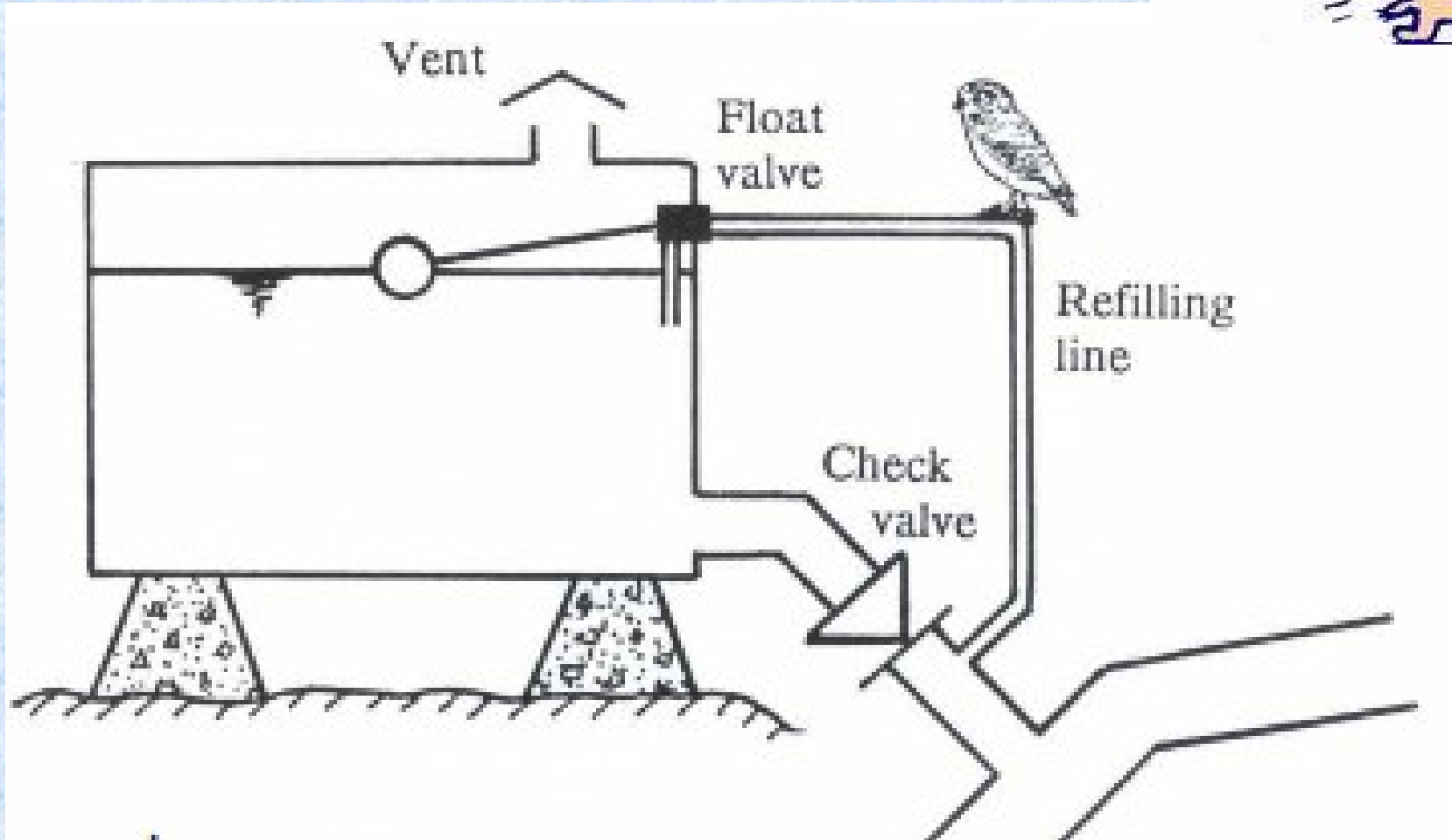
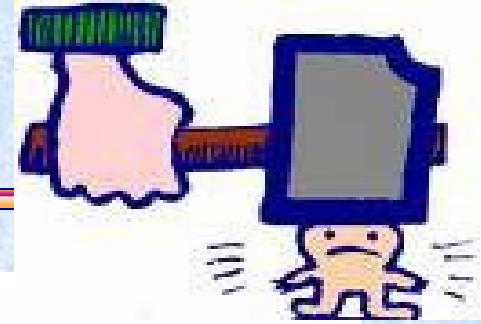
- Simple construction
- Self refilling

### ■ Cons

- Limits negative pressure only
- Risk of water quality problems



# Water Hammer- Mitigation





# Water Hammer- Mitigation



To control minimum pressures, the following can be adjusted or implemented:

- Pump inertia
- Surge tanks
- Air chambers
- One-way tanks
- Air inlet valves
- Pump bypass valves



# Water Hammer- Mitigation



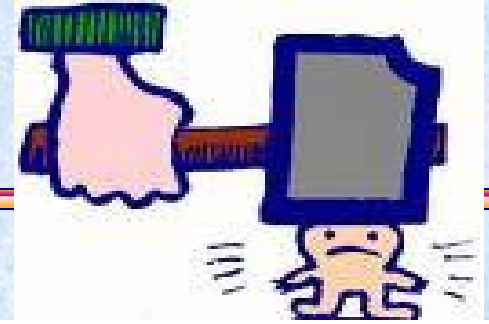
To control maximum pressures, the following can be implemented:

- Relief valves
- Anticipator relief valves
- Surge tanks
- Air chambers
- Pump bypass valves





# Excercise

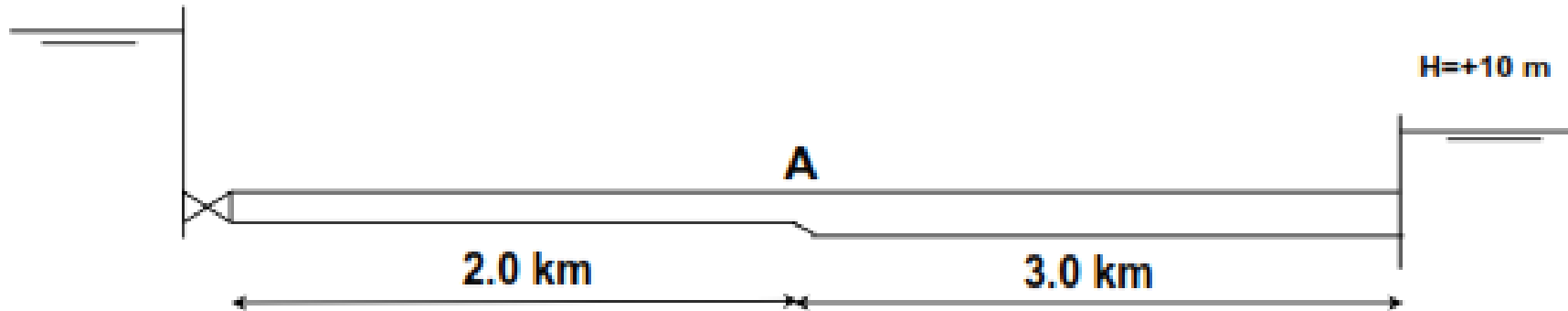


## Fast valve opening

$H = +20$  m

$C = 500$  m/s

$H = +10$  m



$L = 1000$  m

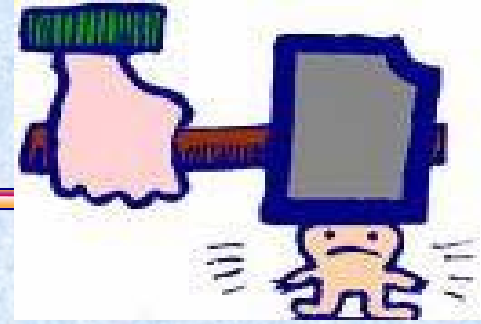
$D_1 = 300$  mm;  $D_2 = 424$  mm

frictionless pipe, conveying water

Draw time graphs of head at 0 km, 2.5 km and 5 km (first 22 s)



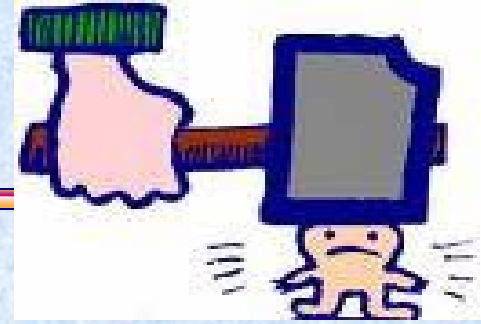
# Excercise



- ❑ 13.1 ( Advanced Water Distribution Modeling)
- ❑ 13.2



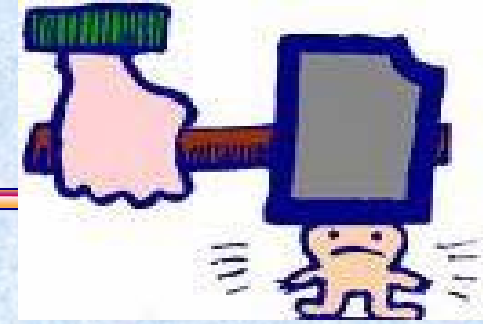
# Exercise



- Derive Joukowski's law from Newton's Second Law of motion. You may assume the wave speed equals  $c$ .



# Information



- WHAMO

- Water Hammer and Mass Oscillation Program

