

## Advanced Process Control CBEg 6142

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## **Chapter 7**

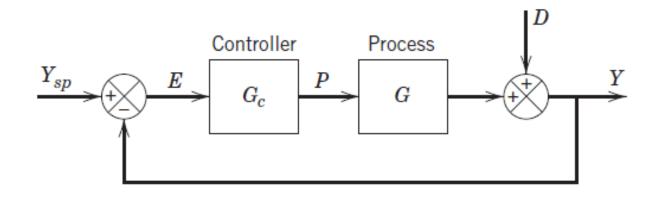
#### **Internal Model Control**



- A more comprehensive model-based design method, Internal Model Control (IMC), was developed by Morari and coworkers (Garcia and Morari, 1982; Rivera et al., 1986).
- The IMC method, like the DS method, is based on an assumed process model and leads to analytical expressions for the controller settings.
- These two design methods are closely related and produce identical controllers if the design parameters are specified in a consistent manner.
- However, the IMC approach has the advantage that it allows model uncertainty and tradeoffs between performance and robustness to be considered in a more systematic fashion.



# Consider the conventional FBC with unmeasured disturbance



It is observed from the block diagram

$$Y = PG + D \tag{7.5}$$



• If the plant model  $\tilde{G}$  is available, the unmeasured disturbance can be estimated from

$$\widetilde{D} = Y - P\widetilde{G} \tag{7.6}$$

• Rearranging (7.6)

$$P = \frac{1}{\tilde{G}} \left( Y - \tilde{D} \right) \tag{7.7}$$

• Assuming ideal controller where  $Y = Y_{sp}$ 

$$P = \frac{1}{\tilde{G}} \left( Y_{sp} - \tilde{D} \right) \tag{7.8}$$

• Defining an internal model control  $(G_{IMC})$  by

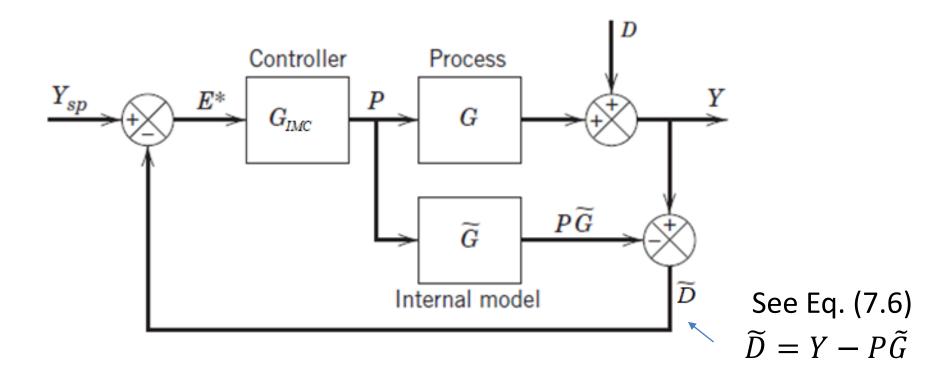
$$G_{IMC} = \frac{1}{\tilde{G}} \tag{7.9}$$

• Using (7.9) in (7.8)

$$P = G_{IMC} \left( Y_{sp} - \widetilde{D} \right) \tag{7.10}$$



• The internal model control can be implemented as shown by the block diagram below

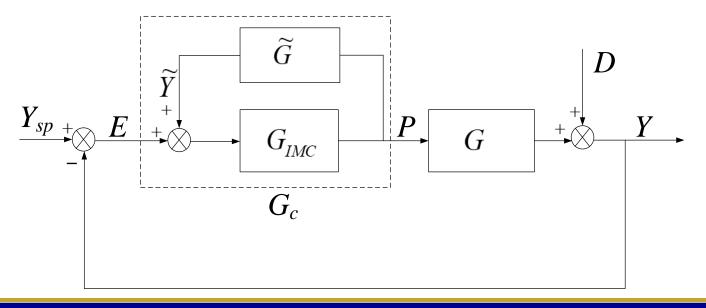


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• From the above block diagram we can derive

$$Y = \frac{G_{IMC}G}{1 + G_{IMC}G}Y_{sp} + \frac{G_{IMC}G}{1 + G_{IMC}G}\tilde{Y} + \frac{1}{1 + G_{IMC}G}D$$
(7.11)

• Eq. (7.11) can be represented by the following equivalent block diagram





• From the last block diagram the relationship between conventional FBC and IMC can be derived

$$EG_c = (E + P\tilde{G})G_{IMC}$$

 $P = EG_c$ 

$$EG_c = (E + EG_c\tilde{G})G_{IMC}$$

$$G_c = \frac{G_{IMC}}{1 - G_{IMC}\tilde{G}}$$



The IMC controller is designed in two steps:

Step 1. The process model is factored as

$$\widetilde{G} = \widetilde{G}_{+} \, \widetilde{G}_{-} \tag{7.12}$$

Where  $\tilde{G}_+$  contains any time delays and right-half plane zeros. In addition  $\tilde{G}_+$  is required to have a steady-state gain equal to one in order to ensure that the two factors in Eq. (7.12) are unique.





• Step 2. The IMC controller is specified as

$$G_{IMC} = \frac{1}{\tilde{G}_{-}}f$$

where *f* is a *low-pass filter* with a steady-state gain of one. It typically has the form

$$f = \frac{1}{(\tau_c s + 1)^n}$$

*n* is selected so that the controller is physically realizable and the desired response is obtained.



#### Example 7.3

For a general first order process and a first order filter derive the IMC controller and the equivalent FBC.

$$\tilde{G} = \frac{K}{\tau s + 1}$$

$$F = \frac{1}{\tau_c s + 1}$$
 Filter



• <u>Solution</u>

$$G_{IMC} = \frac{(\tau s + 1)}{K} \left(\frac{1}{\tau_c s + 1}\right)$$

$$G_{IMC} = \frac{1}{K} \left( \frac{\tau s + 1}{\tau_c s + 1} \right)$$

• The equivalent FBC

$$G_c = \frac{G_{IMC}}{1 - G_{IMC}\tilde{G}}$$



• The equivalent FBC is given by

$$G_{C} = \frac{\frac{1}{K} \left( \frac{\tau s + 1}{\tau_{c} s + 1} \right)}{1 - \frac{1}{K_{p}} \left( \frac{\tau s + 1}{\tau_{c} s + 1} \right) \left( \frac{K}{\tau s + 1} \right)}$$

• After simplification and rearranging we get

$$G_c = \frac{\tau}{K_p \tau_c s} \left( 1 + \frac{1}{\tau s} \right)$$

• This is a PI controller with  $K_c = \tau/(K_p \tau_c)$  and  $\tau_I = \tau$ 



#### Exercise 7.4

For a process that can be approximated a first order plus time delay model derive the IMC controller and the equivalent FBC. Use first order  $\acute{P}$  ade approximation.

$$\tilde{G} = \frac{Ke^{-\theta s}}{\tau s + 1}$$

$$f = \frac{1}{\tau_c s + 1}$$
Filter