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# Advanced Process Control

## CBEg 6142

School of Chemical and Bio-Engineering

Addis Ababa Institute of Technology

Addis Ababa University



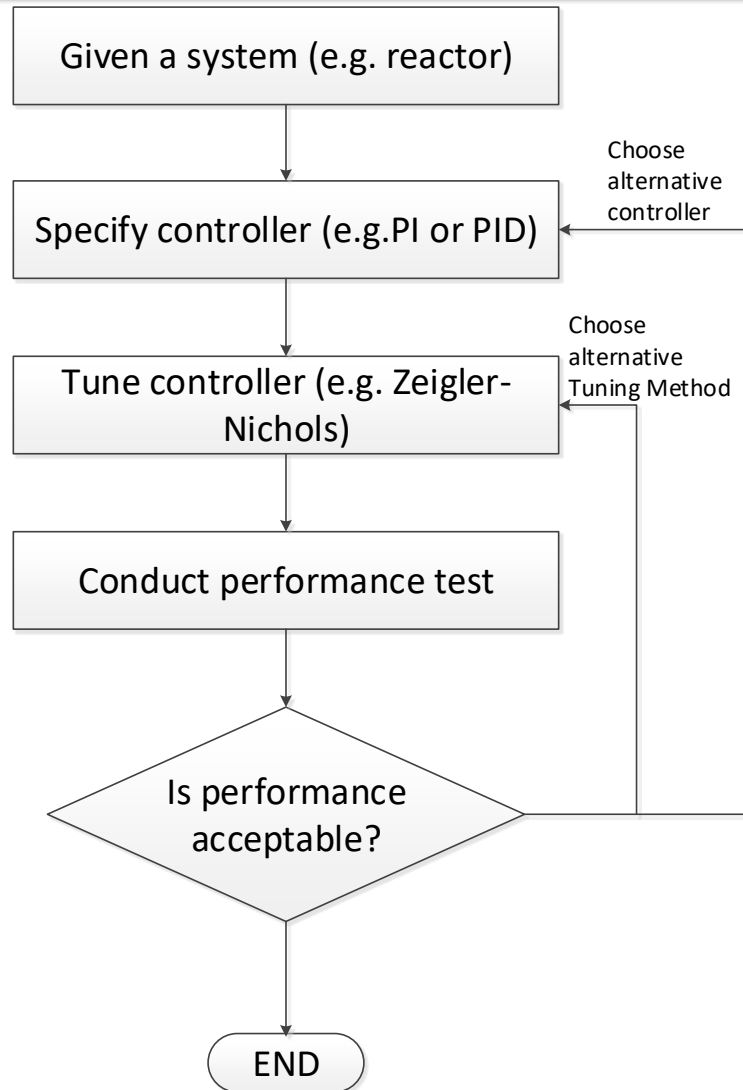
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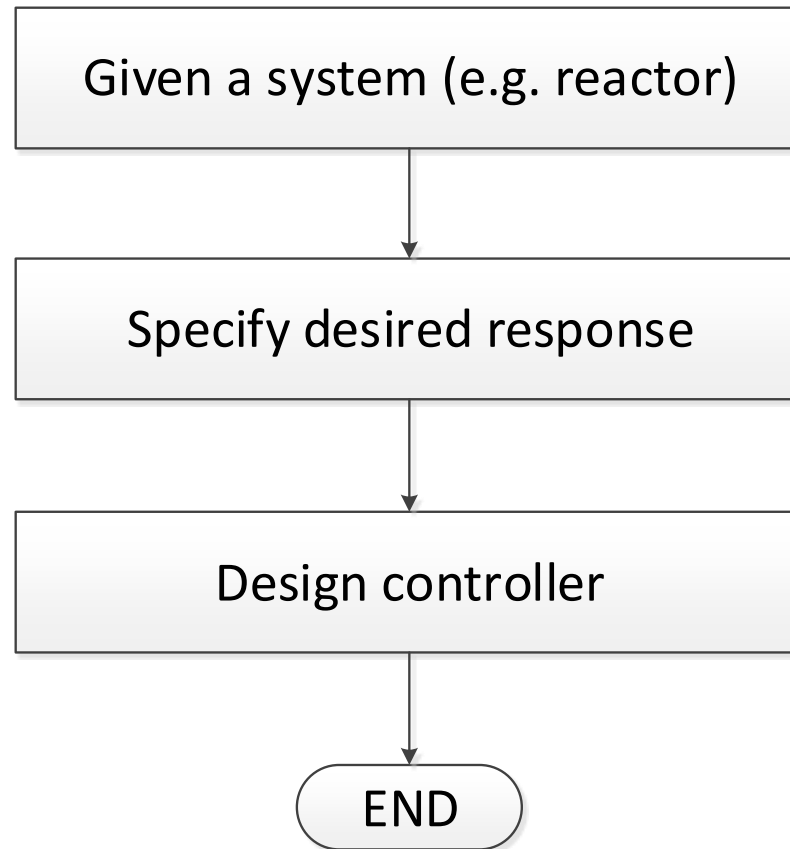
## Chapter 6

# Direct Synthesis Controller

# Controller Design Classical Approach



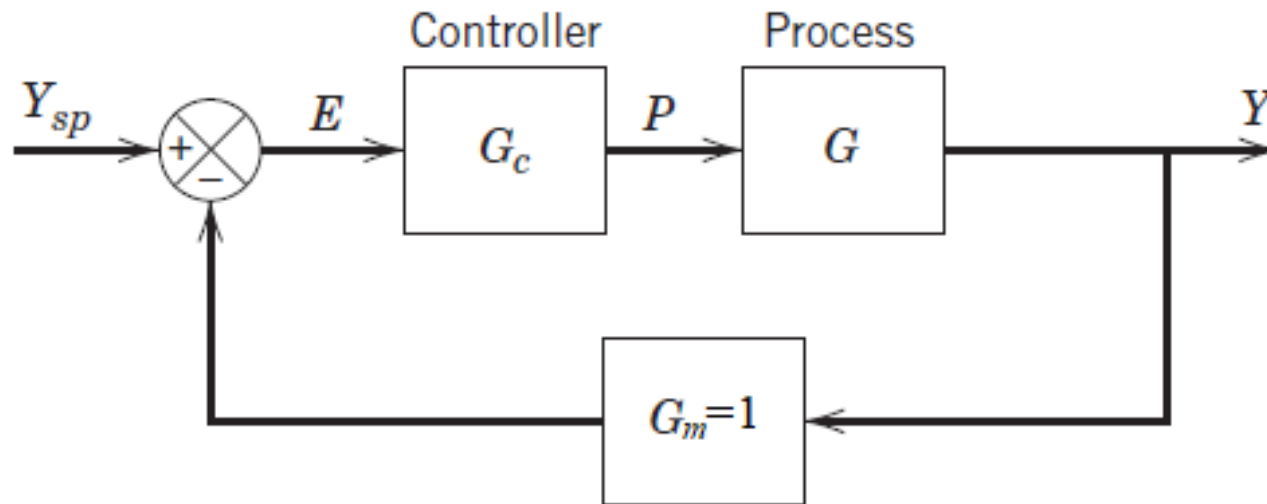
# Direct Synthesis Controller



# Direct Synthesis Controller



The feedback control loop for servo problem



The closed-loop equation for servo problem is given by

$$Y = \frac{G_c G}{1 + G_c G} Y_{sp} \quad (6.1)$$

# Direct Synthesis Controller



Assuming a desired response for  $y(s)$  to be:

$$Y = Q_d Y_{sp} \quad (6.2)$$

Using (6.2) in (6.1)

$$Q_d = \frac{G_c G}{1 + G_c G} \quad (6.3)$$

Rearranging (6.3) we get the design equation

$$G_c = \frac{1}{G} \frac{Q_d}{1 - Q_d} \quad (6.4)$$

# Direct Synthesis Controller



## Example 6.1

The transfer function of a process is given below. The desired closed loop response should have a time constant of 5min and no offset is tolerated. Design a controller using the direct synthesis approach.

$$G = \frac{0.25}{8s + 1}$$
$$Q_d = \frac{1}{5s + 1}$$

No offset

Time constant

# Direct Synthesis Controller



## Solution

$$\begin{aligned}G_c &= \frac{8s + 1}{0.25} \frac{1/(5s + 1)}{1 - 1/(5s + 1)} \\&= \frac{8s + 1}{0.25} \frac{1}{(5s + 1) - 1} \\&= 4 \frac{8s + 1}{5s} \\&= 6.4 \left( 1 + \frac{1}{8s} \right)\end{aligned}$$

This a PI controller with  $K_c=6.4$  and  $\tau_I= 8$  min



# Direct Synthesis Controller



## Example 6.2

The transfer function of a process is given below. The desired closed loop response should have a transfer function given by  $Q_d$ . Design a controller using the direct synthesis approach. Use 1<sup>st</sup> order Taylor series expansion for the time delay.

$$G = \frac{0.2e^{-1.2s}}{3.6s + 1}$$

$$Q_d = \frac{e^{-1.2s}}{s + 1}$$

# Direct Synthesis Controller



## Solution

$$G_c = \frac{(3.6s + 1)}{0.2} \frac{e^{-1.2s}/(s + 1)}{1 - e^{-1.2s}/(s + 1)}$$

$$= \frac{(3.2s + 1)}{0.2} \frac{1}{s + 1 - e^{-1.2s}}$$

$$= \frac{(3.2s + 1)}{0.2} \frac{1}{s + 1 - (1 - 1.2s)}$$

$$G_c = \frac{(3.2s + 1)}{0.44s} = \frac{3.2}{0.44} \left( 1 + \frac{1}{3.2s} \right) = 7.27 \left( 1 + \frac{1}{3.2s} \right)$$

This a PI controller with  $K_c = 7.27$  and  $\tau_i = 3.2$  min

# Direct Synthesis Controller



## Example 6.3

For process that are estimated by first order plus time delay (FOPTD) and second order plus time delay (SOPTD) models given below. Design controllers using the direct synthesis approach. Use 1<sup>st</sup> order Taylor series expansion for the time delay.

$$G = \frac{K e^{-\theta s}}{\tau s + 1}$$

$$G = \frac{K e^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)}$$

# Direct Synthesis Controller



## Solution

$$Q_d = \frac{1e^{-\theta s}}{\tau_c s + 1}$$

$$G = \frac{Ke^{-\theta s}}{\tau s + 1}$$

$$G_c = \frac{\tau s + 1}{Ke^{-\theta s}} \frac{\frac{1e^{-\theta s}}{\tau_c s + 1}}{1 - \frac{1e^{-\theta s}}{\tau_c s + 1}} = \frac{\tau s + 1}{K} \frac{1}{\tau_c s + 1 - e^{-\theta s}}$$

Using first order Taylor's expansion  $e^{-\theta s} = 1 - \theta s$

$$G_c = \frac{\tau s + 1}{K(\tau_c + \theta)s} = \frac{\tau}{K(\tau_c + \theta)} \left( 1 + \frac{1}{\tau s} \right)$$

This is a PI controller with  $K_c = \frac{\tau}{K(\tau_c + \theta)}$  and  $\tau_I = \tau$

# Direct Synthesis Controller



## Solution

$$Q_d = \frac{1e^{-\theta s}}{\tau_c s + 1}$$

$$G = \frac{Ke^{-\theta s}}{(\tau_1 s + 1)(\tau_2 s + 1)}$$

Inserting and simplifying

$$G_c = \frac{\tau_1 \tau_2 s^2 + (\tau_1 + \tau_2)s + 1}{K(\tau_c + \theta)s} = \frac{\tau_1 + \tau_2}{K(\tau_c + \theta)} + \frac{1}{K(\tau_c + \theta)s} + \frac{\tau_1 \tau_2}{K(\tau_c + \theta)} s$$

$$G_c = \frac{\tau_1 + \tau_2}{K(\tau_c + \theta)} \left( 1 + \frac{1}{(\tau_1 + \tau_2)s} + \frac{\tau_1 \tau_2}{\tau_1 + \tau_2} s \right)$$

This is a PID controller with  $K_c = \frac{\tau_1 + \tau_2}{K(\tau_c + \theta)}$   $\tau_I = \tau_1 + \tau_2$  and  $\tau_D = \frac{\tau_1 \tau_2}{\tau_1 + \tau_2}$

# Direct Synthesis Controller



## Exercise 6.1

The transfer function of three processes are given below. The desired closed loop response should have no-offset. For each of the three processes design a controller using the direct synthesis approach. Determine, the time desired time constant by yourself. Use Skogestad's half rule whenever necessary.

$$i. \quad G = \frac{3.5(-0.5s+1)e^{-0.8s}}{(4.2s+1)(3.2s+1)}$$

$$ii. \quad G = \frac{0.5e^{-1.4s}}{(4.2s+1)(1.7s+1)(0.8s+1)}$$

$$iii. \quad G = \frac{0.5(-0.8s+1)e^{-1.4s}}{(4.2s+1)(1.7s+1)(0.8s+1)}$$